

### PRUET PRODUCTION CO.

217 WEST CAPITOL STREET / SUITE 201 • JACKSON, MISSISSIPPI 39201

January 9, 2023

Ms. Krystal Rudolph, P.E. Chief Environmental Permits Division Mississippi Department of Environmental Quality PO Box 2261 Jackson, MS 39225-2261

Dear Ms. Rudolph:

Re: Pruet Production Company. Board of Education 16-10 No. 1 Facility AI# 72370, Permit No. 2420-00053 Scott County, MS

Pruet. Production Company is submitting the enclosed completed request for coverage under the Mississippi Oil Production General Permit in lieu of a renewal application for the Synthetic Minor Operating Permit which expires July 31, 2023.

If you have any questions, please feel free to contact me at (601) 718-9423 or Toby Cook at (601) 613-1915.

J. David Hilton

Sincere

Vice President-Production

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Dept. of Environmental Quality

#### Oil Production General Permit Public Notice Mississippi Environmental Quality Permit Board P. O. Box 2261 Jackson, Mississippi 39225 Telephone No. (601) 961-5171

#### Public Notice Start Date: 1/18/2023

Pruet Production Company Board of Education 16-10 No. 1 facility located at Lat.32.27460, Long-89.68685, Scott County, MS, approximately 5.5 miles southwest of Morton, MS, in Section 16, T5N, R6E, (601) 748-9423, has applied to the Mississippi Department of Environmental Quality (MDEQ) for coverage under MDEQ's Oil Production General Permit to operate an oil production facility.

The Oil Production General Permit has been developed to ensure compliance with all State and Federal regulations. Facilities granted coverage under this permit and adhering to the conditions contained therein should operate within State and Federal environmental laws and standards concerning the operation of air emissions equipment.

The existing facility currently operates under Air permit No. 2420-00053 and consists of an oil and gas production site including well, oil and water storage tanks, electric well pump, and a flare to control gas emissions. Pruet is requesting a federally enforceable permit requirement that the storage tank emissions be routed to the flare at all times the facility is in operation. The facility will operate control(s) such that criteria pollutant emissions will not exceed emission rates restricted in the Oil Production General Permit, nor will hazardous air pollutant (HAP) emissions exceed any HAP emission rates restricted in the Oil Production General Permit. This project will result in new sources of potential emissions of regulated air pollutants. However, emissions will be below the Prevention of Significant Deterioration significance levels as specified in the Mississippi Regulations for the Prevention of Significant Deterioration of Air Quality, 11 Miss. Admin. Code Pt. 2, Ch. 5., and in 40 CFR Part 52.21. Potential emissions will also be below the Air Title V Major Source thresholds as specified in 11 Miss. Admin. Code Pt. 2, Ch. 6. and in 40 CFR Part 70.

Persons wishing to comment upon or object to the proposed request are invited to submit comments in writing to the **Air 1 Branch Chief, Environmental Permits Division** at the Permit Board's address shown above no later than 30-days from the date of publication of this notice. All comments received or postmarked by this date will be considered in the determination regarding the coverage approval. After receipt of public comments and thorough consideration of all comments, MDEQ will formulate its recommendations regarding coverage approval.

Additional details about the proposed project are available by writing or calling the **Air 1 Branch Chief, Environmental Permits Division** at the above Permit Board address and telephone number and on the MDEQ's website at: <a href="https://www.mdeq.ms.gov/ensearch/recently-received-general-permit-noi/">https://www.mdeq.ms.gov/ensearch/recently-received-general-permit-noi/</a>. This information is also available for review at the following locations during normal business hours:

Mississippi Department of Environmental Quality
Office of Pollution Control
515 East Amite Street,
Jackson, MS 39201
(601) 961-5171

Morton Public Library 16 E. Fourth Ave. Morton, MS 39117

Please bring the foregoing to the attention of persons whom you know will be interested.

# OIL PRODUCTION GENERAL PERMIT NOTICE OF INTENT



Pruet Production Company Board of Education 16-10 No. 1 Facility Scott County, Mississippi

Submittal Date: January 2023

PREPARED BY:

FC&E ENGINEERING, LLC

917 MARQUETTE ROAD BRANDON, MISSISSIPPI 39042 (601) 824-1860



#### **EXECUTIVE SUMMARY**

Pruet Production Company (Pruet) is submitting this Notice of Intent for the purpose of replacing the SMOP for the Pruet Board of Education 16-10 facility located in Scott county. The facility is located in Section 24, Township 3N, Range 5E, in Scott County, Mississippi. The facility now includes the well, an electric power-oil pump, crude oil and produced water storage tanks, and a flare. The heater treater, which was never connected to a fuel supply, has been bypassed so that all gas emissions are emitted from the storage tanks. This change in operation was required due to the decline in oil and gas production as the well transitioned from a flowing well to a well produced by pumping. Production rates are typically 30 to 40 thousand cubic feet (MCF) of gas produced per day and 35 to 40 barrels (bbl) of oil produced per day, along with 1 bbl/day or less of produced water. A pipeline outlet does not exist for the gas; therefore, all gas is flared.

Pruet is requesting a federally enforceable requirement for flaring of tank emissions. Emissions associated with truck loading will be vented to the atmosphere. Pruet may also operate various small chemical storage vessels, including totes and drums, which are typically associated with well pad activities.

Consequently, Pruet is submitting the attached Notice of Intent (NOI) and associated information for issuance of coverage under the Oil Production General Permit. Based on the facility's potential to emit, the facility's uncontrolled potential emissions of Volatile Organic Compounds (VOC) exceed the threshold limit to be classified as a True Minor Source. Therefore, Pruet proposes to restrict facility operations such that the flare is operated at all times during gas venting. Combustion of produced gas from the well, which vents from the power oil tank, and gas off of the other oil and water storage tanks will ensure VOC emissions from the facility do not exceed the Air Title V Major Source threshold of 100 tons per year and the General permit limit of 95 tons per year. Pruet will monitor the volume of gas flared using an approved calculation methodology due to the difficulty in utilizing a flow meter on atmospheric pressure tanks. Pruet will calculate corresponding monthly VOC emissions due to flaring of gas from all sources. Monthly oil production records, gas sampling and E&P TANKS software will be utilized to calculate emissions from the storage tanks to the flare. Emissions calculations will be maintained on a monthly and rolling, consecutive 12-month basis to ensure compliance with permitted emissions thresholds.

Also included with the NOI are associated maps and figures. Detailed air emissions calculations are provided in Appendix A, and pertinent backup documentation is provided in Appendix B.

# MDEQ NOTICE OF INTENT FOR COVERAGE UNDER THE OIL PRODUCTION GENERAL PERMIT TO CONSTRUCT/OPERATE AIR EMISSIONS EQUIPMENT AT A SYNTHETIC MINOR SOURCE

Facility (Agency Interest) Information		Section OPGP - A
1. Name, Address, and Location of Facility		
A. Owner/Company Name: Pruet Prod	luction Company	
B. Facility Name (if different than A. above):	Board of Education 16-10	O No. 1 DE GE
C. Facility Air Permit/Coverage No. (if known)	: 2420-00053	JAN 1 0
D. Agency Interest No. (if known):	723	70
E. Physical Address 1. Street Address: 5629 Highway 13 Sou	ıth	MDE
2. City: Morton	3. State:	MS
4. County: Scott	5. Zip Code: 3	39117
6. Telephone No.: 601-748-9423	7. Fax No.:	
8. Are facility records kept at this location?	<del>-</del>	ease complete Item 10.
F. Mailing Address  1. Street Address or P.O. Box: 217 W Car  2. City: Jackson  4. Zip Code: 39201  G. Latitude/Longitude Data  1. Collection Point (check one):  Site Entrance  2. Method of Collection (check one):  GPS Specify coordinate system of the property of the pr	Other: well location stem (NAD 83, etc.)	Other:
H. SIC Code: <u>1311</u>	_	
2. Name and Address of Facility Contact		
A. Name: J. David Hilton	Title:	VP-Production
	pital Suite 201  3. State:	MS
Backs December 2 on American September 2	<b>■</b> ()	VIS
4. Zip Code: 39201	5. Fax No.: _	
6. Telephone No.: 601-748-9423 7. Email: dhilton@pruet.com	-	

## MDEQ NOTICE OF INTENT FOR COVERAGE UNDER THE OIL PRODUCTION GENERAL PERMIT TO CONSTRUCT/OPERATE AIR EMISSIONS EQUIPMENT AT A SYNTHETIC MINOR SOURCE

Facility (Agen	cy Interest) Information			Section OPGP - A
3. Name and A	Address of Air Contact (if different fr	om I	Facility Con	tact)
A. Name:			Title:	
B. Mailing	Address dress or P.O. Box:			
2. City:	uless of 1.0. Box.		3. State:	<del></del>
4. Zip Code:	•		5. Fax No.:	
6. Telephone			3. I da 110	
7. Email:				
4. Name and A	Address of Responsible Official for the	ne Fa	acility	
The Form must	be signed by a Responsible Official as defin	ied in	11 Miss. Adm	in. Code Pt.2, R. 2.1.C(24).
A. Name:	J. David Hilton		Title:	VP-Production
B. Mailing A	Address			
1. Street Ad	dress or P.O. Box: 217 W. Capital S	treetS	Suite 201	
2. City:	Jackson		3. State:	MS
4. Zip Code:	39201		5. Fax No.:	
6. Telephone				
7. Email:	dhilton@pruet.com			
C. Is the per	son above a duly authorized representative Yes   No	e and	not a corpora	ite officer?
If yes, has w	ritten notification of such authorization be	een s	ubmitted to M	IDEQ?
	Yes		Request for a	authorization is attached
5. Type of Oil	Production Notice of Intent (Check of	all th	at apply)	
<b>V</b>	Initial Coverage		Re-Coverage	e for existing Coverage
	Modification with Public Notice		Modification	without Public Notice
	Update Compliance Plan			

## MDEQ NOTICE OF INTENT FOR COVERAGE UNDER THE OIL PRODUCTION GENERAL PERMIT TO CONSTRUCT/OPERATE AIR EMISSIONS EOUIPMENT AT A SYNTHETIC MINOR SOURCE

	QUIPMENT AT A SYNTHETIC MI	HOR SOURCE
Facility (Agency Interest	t) Information	Section OPGP - A
6. Equipment List (Chec	k all that apply )	
Complete supporting emission	n calculations must be included for each potential o	emission unit selected below.
<del>-</del>		ļ
_	a completed <u>Section OPGP-C Form</u> for each unit	
	essel. Include a completed Section OPGP-E Forn	
	nclude a completed <u>Section OPGP-E Form</u> for ea	
	gine. Include a completed Section OPGP-D Form	1 for each unit.
•	ted Section OPGP-F Form for each unit.	!
Oil Truck Loading (Sect		
	nissions ( <u>Section OPGP-B Form</u> )	
Other:		
= M /D d 4 Do4o!		
7. Process/Product Detai	ls	
Ma	eximum Anticipated Well(s) Production for Facil	4:.,,
Produced Material	Throughput	Units
Gas	60	MMCF/day
Oil	66	barrels/day
Water	1	barrels/day
Other (Specify)		
<u> </u>	<u> </u>	<u> </u>
Maximum An	aticipated Throughput for Principal Product(s) (as	s applicable ):
Produced Material	Throughput	Units
Flared Gas	60	MMCF/day
Oil	66	barrels/day
Water	1	barrels/day
Other (Specify)		
8. Zoning		
- ,	sting or proposed) located in accordance with any	y applicable city and/or
county zoning ordinance	es? If no, please explain	
Yes		
D. J. des Carilles (aithan ani)	No control to the least one on the	•
· · · · · · · · · · · · · · · · · · ·	sting or proposed) required to obtain any zoning	variance to
•	y at this site? If yes, please explain.	
No		
C Is the required USGS on	adrangle map or equivalent attached?	✓ Yes ☐ No
C. Is the required 0505 qu	aurangle map or equivalent attacheu:	L ICS L INU

## MDEQ NOTICE OF INTENT FOR COVERAGE UNDER THE OIL PRODUCTION GENERAL PERMIT TO CONSTRUCT/OPERATE AIR EMISSIONS EQUIPMENT AT A SYNTHETIC MINOR SOURCE

Facility (Agency Interest) Information

Section OPGP - A

9. MS Secretary of State Registration / Certificate of Good Standing

No permit will be issued to a company that is not authorized to conduct business in Mississippi. If the company applying for the permit is a corporation, limited liability company, a partnership or a business trust, the application package should include proof of registration with the Mississippi Secretary of State and/or a copy of the company's Certificate of Good Standing. The name listed on the permit will include the company name as it is registered with the Mississippi Secretary of State.

It should be noted that for an application submitted in accordance with 11 Miss. Admin. Code Pt. 2, R. 2.8.B. to renew a State Permit to Operate or in accordance with 11 Miss. Admin. Code Pt. 2, R. 6.2.A(1)(c). to renew a Title V Permit to be considered timely and complete, the applicant shall be registered and in good standing with the Mississippi Secretary of State to conduct business in Mississippi.

· · · · · · · · · · · · · · · · · · ·	217 W. Capital Street, S 601-748-9423	3. State: MS 5. Zip Code: 39201 7. Fax No.:		
		5. Zip Code: 39201		
· -	601-748-9423		39201	
relepnone No.:	601-748-9423	/. Fax No.:		

## MDEQ NOTICE OF INTENT FOR COVERAGE UNDER THE OIL PRODUCTION GENERAL PERMIT TO CONSTRUCT/OPERATE AIR EMISSIONS EQUIPMENT AT A SYNTHETIC MINOR SOURCE

Facility	(Agency	Interest)	Information
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Section OPGP - A

#### 11. Certification

The Form must be signed by a Responsible Official as defined in 11 Miss. Admin. Code Pt. 2, R. 2.1.C.(24).

I certify that to the best of my knowledge and belief formed after reasonable inquiry, the statements and information in this application are true, complete, and accurate, and that as a responsible official, my signature shall constitute an agreement that the applicant assumes the responsibility for any alteration, additions, or changes in operation that may be necessary to achieve and maintain compliance with all applicable Rules and Regulations. I am aware that there are significant penalties for submitting false information, including the possibility of fine and imprisonment.

Signature of Responsible Official/DAR

J. David Hilton

**Printed Name** 

#### Section B.1: Maximum Uncontrolled Emissions (under normal operating conditions)

Maximum Uncontrolled Emissions are the emissions at maximum capacity and prior to (in the absence of) pollution control, emission-reducing process equipment, or any other emission reduction. Calculate the hourly emissions using the worst case hourly emissions for each pollutant. For each pollutant, calculate the annual emissions as if the facility were operating at maximum plant capacity without pollution controls for 8760 hours per year, unless otherwise approved by the Department. List Hazardous Air Pollutants (HAP) in Section B.4. Emission Point numbering must be consistent throughout the application package and, for existing emission points, should match any MDEQ ID's in the current permit. Fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected. Emissions > 0.01 TPY must be included. Please do not change the column widths on this table.

Emission	TSP	(PM)	PM	-10 <sup>1</sup>	PM-	·2.5¹	Ŝ	02	N	Ox	C	O	V	OC .	TI	RS²	Le	ad	Total	HAPs
Point ID	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	Murry	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/br	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
AA-001	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	54.94	240.62	0.00	0.00	0.00	0.00	2.7563	12.0725
AA-003	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0,00	0.00	0.00	0.00	0.00	0.08	0.33	0.00	0.00	0.00	0,00	0.0052	0.0228
AA-005	-	_	_	-	•	-	1	1	_	-	-	-	0.05	0.20	1	-	_	_	0.0000	0.0200
AA-006	Routed to	AA-001																	* .	
AA-007	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.02	0.00	0.00	0,00	0.00	0.0043	0.0190
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Totals	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	55.06	241.17	0.00	0.00	0.00	0.00	2.77	12.13

<sup>&</sup>lt;sup>1</sup> Condensables: Include condensable particulate matter emissions in particulate matter calculations for PM-10 and PM-2.5, but not for TSP (PM).

<sup>&</sup>lt;sup>2</sup> TRS: Total reduced sulfur (TRS) is the sum of the sulfur compounds hydrogen sulfide (H<sub>2</sub>S), methyl mercaptan (CH<sub>4</sub>S), dimethyl sulfide (C<sub>2</sub>H<sub>6</sub>S), and dimethyl disulfide (C<sub>2</sub>H<sub>6</sub>S<sub>2</sub>).

#### Section B.2: Proposed Allowable Emissions

Proposed Allowable Emissions (Potential to Emit) are those emissions the facility is currently permitted to emit as limited by a specific permit requirement or federal/state standard (e.g., a MACT standard); or the emission rate at which the facility proposes to emit considering emissions control devices, restrictions to operating rates/hours, or other requested permit limits that reduce the maximum emission rates. Emission Point numbering must be consistent throughout the application package and, for existing emission points, should match any MDEQ ID's in the current permit. Fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected. Additional columns may be added if there are regulated pollutants (other than HAPs and GHGs) emitted at the facility.

Emission								t the racin		<u> </u>		O.	12	20		DC		
		SP <sup>1</sup>		1101		2.5 <sup>1</sup>				Ox				OC		RS		ad
Point ID	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/br	ton/yr
AA-001	0.01	0.03	0.03	0.12	0.03	0.12	0.00	0.00	0.24	1.06	1.11	4.84	1.10	4.81	0.00	0.00	0.00	0.00
AA-003	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0,00	0.00	0.00	0.00	0.00	0.06	0.28	0.00	0.00	0.00	0.00
AA-005	_				_	_	_	_	_		_		0.05	0.20	-	_	-	-
AA-006	Routed to	AA-001																
AA-007	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.02	0.00	0.00	0.00	0.00
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Totals	0.01	0.03	0.03	0.12	0.03	0.12	0.00	0.00	0.24	1.06	1.11	4.84	1.22	5.31	0.00	0.00	0.00	0.00

<sup>1</sup> Condensables: Include condensable particulate matter emissions in particulate matter calculations for PM-10 and PM-2.5, but not for TSP (PM).

<sup>&</sup>lt;sup>2</sup> TRS: Total reduced sulfur (TRS) is the sum of the sulfur compounds hydrogen sulfide (H<sub>2</sub>S), methyl mercaptan (CH<sub>4</sub>S), dimethyl sulfide (C<sub>2</sub>H<sub>6</sub>S), and dimethyl disulfide (C<sub>2</sub>H<sub>6</sub>S<sub>2</sub>).

#### Section B.3: Proposed Allowable Hazardous Air Pollutants (HAPs)

In the table below, report the Proposed Allowable Emissions (Potential to Emit) for each HAP from each regulated emission unit if the HAP > 0.0001 tpy. Each facility-wide Individual HAP total and the facility-wide Total HAPs shall be the sum of all HAP sources. Use the HAP nomenclature as it appears in the Instructions. Emission Point numbering must be consistent throughout the application package and, for existing emission points, should match any MDEQ ID's in the current permit. For each HAP listed, fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected or the pollutant is emitted in a quantity less than the threshold amounts described above. Additional columns may be added as necessary to address each HAP.

	ission Total HAPs   1,1,2,2-   1,1,2,2-   1,1,2,4-richtoroethane   1,3-butadiene   1,3-dichloropropene   acetaldehyde   acrolein   benzene   carbon t																	
Emission	Total	HAPs	tetrachio		1,1,2-trich	loroethane	1,3-bu	tadiene	1,3-dichle	горгорепе	acetal	dehyde	acr	olein	ben	zene	carbon te	trachloride
Point ID	lb/hr	ton/yr	ib/br	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
AA-001	0.05512	0.24145	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	0.00515	0.02255	<0.0001	<0.0001
AA-003	0.00364	0.02275	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	0.00022	0.00095	<0.0001	<0.0001
AA-005	0.05	0.02		_		-	_	_	_	-	_	-	_		1	_	-	
AA-006	Routed to	AA-001																
AA-007	0.00434	0.019	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001
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Totals:	0.1131	0.3032	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0054	0.0235	0.0000	0.0000

#### Section B.3: Proposed Allowable Hazardous Air Pollutants (HAPs)

In the table below, report the Proposed Allowable Emissions (Potential to Emit) for each HAP from each regulated emission unit if the HAP > 0.0001 tpy. Each facility-wide Individual HAP total and the facility-wide Total HAPs shall be the sum of all HAP sources. Use the HAP nomenclature as it appears in the Instructions. Emission Point numbering must be consistent throughout the application package and, for existing emission points, should match any MDEQ ID's in the current permit. For each HAP listed, fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected or the pollutant is emitted in a quantity less than the threshold amounts described above. Additional columns may be added as necessary to address each HAP.

Emission	Total	HAPs	chlorot	enzene	chlor	oform	cthy lb	enzene	ethylene o	libromide	formal	dehyde	met	anol	methylen	e chloride	napht	halene
Point ID	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/br	ton/yr	lb/hr	ton/yr
AA-001	0.1414	0.2415	<0.0001	<0.0001	<0.0001	<0.0001	0.00457	0.02001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001
AA-003	0.00519	0.02275	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	0.00102	<0.0001	<0.0001	<0.0001	<0,0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001
AA-005	_	_	-	_	_	_	_	_	_	-	-	-	_	_	-	_	_	
AA-006	Routed to	AA-001																
AA-007	0.0043	0.0190	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001
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Totals:	0.1509	0.2832	0.0000	0.0000	0.0000	0.0000	0.0046	0.0210	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000

#### Section B.3: Proposed Allowable Hazardous Air Pollutants (HAPs)

In the table below, report the Proposed Allowable Emissions (Potential to Emit) for each HAP from each regulated emission unit if the HAP > 0.0001 tpy. Each facility-wide Individual HAP total and the facility-wide Total HAPs shall be the sum of all HAP sources. Use the HAP nomenclature as it appears in the Instructions. Emission Point numbering must be consistent throughout the application package and, for existing emission points, should match any MDEQ ID's in the current permit. For each HAP listed, fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected or the pollutant is emitted in a quantity less than the threshold amounts described above. Additional columns may be added as necessary to address each HAP.

Emission	Total	HAPs	P/	AH .	styr	rene	tolu	ene	vinyl c	hloride	xyl	lene	hex	ane	PC	DM MC	-	
Point ID	lb/hr	ton/yr	lb/br	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/br	ton/yr
AA-001	0.14138	0.24145	<0.0001	<0.0001	<0.0001	<0.0001	0.00183	0.00799	<0.0001	<0.0001	0.0014	0.00612	0.04219	0.18478	<0.0001	<0.0001		
AA-003	0.00519	0.02275	<0.0001	<0.0001	<0.0001	<0.0001	3.6E-05	0.00016	<b>√0.0001</b>	<0.0001	3.6E-05	0.00016	0.00186	0.00814	<0.0001	<0.0001		
AA-005	<u> </u>	-	-	-	ı	•	0.00	0.02	ı	_	_	-	ı	1	1	_		
AA-006	Routed to	AA-001																
AA-007	0.00434	0.019	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001		
																ļ		
																		igwdot
											<u> </u>							igsquare
		-														-		
									-			<b>-</b>						
												-			-			
Totals:	0.1509	0.2832	0.0000	0.0000	0.0000	0.0000	0.0064	0.0282	0.0000	0.0000	0.0014	0.0063	0.0440	0.1929	0.0000	0.0000		

#### Section B.4: Greenhouse Gas Emissions

Applicants must report potential emission rates in SHORT TONS per year, as opposed to metric tons required by Part 98. Emission Point numbering must be consistent throughout the application package and for existing emission points, should match any MDEO ID's in the current permit.

		CO <sub>2</sub> (non- biogenic) ton/yr	CO <sub>2</sub> (biogenic) <sup>2</sup> ton/yr	N <sub>2</sub> O ton/yr	CH <sub>4</sub> ton/yr	SF <sub>6</sub> ton/yr	PFC/HFC <sup>3</sup> ton/yr				Total GHG Mass Basis ton/yr <sup>5</sup>	Total CO2e ton/yr <sup>6</sup>
Emission Point ID	GWPs 1	1	1	298	25	22,800	footnote 4					
AA-001	mass GHG	1907.95	0	0.00	5.73	0	0				1913.68	N/A
AA-001	CO2e	1907.95	0	0.91	143.15	0	0				N/A	2052.02
AA-003	mass GHG	0	0	0	0	0	0				0.25	N/A
727-000	CO2e	0	0	0	6	0	0				N/A	6.21
AA-005	mass GHG	0	0	0	0	0	0				0.00	N/A
121-000	CO2e	0	0	0	0	0	0	l		<u> </u>	N/A	0.00
AA-006	mass GHG	0	0	0	0	0	0				0.00	N/A
7474-000	CO <sub>2</sub> e	0	0	0	0	0	0			<u>L</u>	N/A	0.00
AA-007	mass GHG	0	0	0	0	0	0				0.00	N/A
AA-007	CO <sub>2</sub> e	0	0	0	0	0	0				N/A	0.00
				_								
								-				
FACILITY	mass GHG	1907.95	0	0.00	5.97	0.00	0.00				1913.93	N/A
TOTAL	COre	1907.95	0	0.91	149.36	0.00	0.00		1		N/A	2058.23

<sup>&</sup>lt;sup>1</sup> GWP (Global Warming Potential): Applicants must use the most current GWPs codified in Table A-1 of 40 CFR part 98. GWPs are subject to change, therefore, applicants need to check 40 CFR 98 to confirm GWP values.

<sup>&</sup>lt;sup>2</sup> Biogenic CO2 is defined as carbon dioxide emissions resulting from the combustion or decomposition of non-fossilized and biodegradable organic material originating from plants, animals, or micro-organisms.

<sup>&</sup>lt;sup>3</sup> For HFCs or PFCs describe the specific HFC or PFC compound and use a separate column for each individual compound.

<sup>&</sup>lt;sup>4</sup> For each new compound, enter the appropriate GWP for each HFC or PFC compound from Table A-1 in 40 CFR 98.

<sup>&</sup>lt;sup>5</sup> Greenhouse gas emissions on a mass basis is the ton per year greenhouse gas emission before adjustment with its GWP. Do not include biogenic CO<sub>2</sub> in this total.

<sup>&</sup>lt;sup>6</sup> CO<sub>2</sub>e means Carbon Dioxide Equivalent and is calculated by multiplying the TPY mass emissions of the greenhouse gas by its GWP. Do not include biogenic CO<sub>2</sub>e in this total.

#### Section B.5: Stack Parameters and Exit Conditions

Emission Point numbering must be consistent throughout the application package and, for existing emission points, should match any MDEQ ID's in the current permit.

Emission Point ID	Orientation (H- Horizontal	Rain Caps	Height Above Ground	Base Elevation	Exit Temp.	Inside Diameter or Dimensions	Velocity	Moisture by Volume		ic Position utes/seconds)
roint 1D	V=Vertical)	(Yes or No)	(ft)	(ft)	(°F)	(ft)	(ft/sec)	(%)	Latitude	Longitude
AA-001	Н	No	40	415	1800	0.50	100	TBD	32/16/29.172N	89/41/12.84W
			<u> </u>					<u> </u>		
AA-003	N/A-Fugitives	N/A	N/A	415	N/A	N/A	N/A	N/A	32/16/29.172N	89/41/12.84W
AA-005	N/A Misc Tanks	N/A	N/A	415	N/A	N/A	N/A	N/A	32/16/29.172N	89/41/12.84W
AA-006	N/A Tanks	N/A	N/A	415	N/A	N/A	N/A	N/A	32/16/29.172N	89/41/12.84W
AA-007	N/A-Loading	N/A	N/A	415	N/A	N/A	N/A	N/A	32/16/29.172N	89/41/12.84W
				i		1		<u> </u>		

<sup>&</sup>lt;sup>1</sup> A WAAS-capable GPS receiver should be used and in the WGS84 or NAD83 coordinate system.

#### MDEQ NOTICE OF INTENT FOR COVERAGE UNDER THE OIL PRODUCTION GENERAL PERMIT TO CONSTRUCT/OPERATE AIR EMISSIONS EQUIPMENT AT A SYNTHETIC MINOR SOURCE Flare **Section OPGP-F Equipment Description** Emission Point Designation (Ref. No.): AA-001 B. Equipment Description (include the process(es) that the flare controls emissions from): Flare controls gas produced/emissions from 3 crude storage tanks, 1 produced water storage tank. Flare is designed in accordance with 40 CFR 60.18 for gas velocity and heat content of flared gas. C. Manufacturer: custom D. Model: custom E. Status: M Operating Proposed **Under Construction** F. Requesting a federally enforceable condition to route tank emissions to the flare. 2. System Data Controlling the following pollutant(s): VOC A. Efficiency: Efficiency: Controlling the following pollutant(s): Reason for different efficiency: Flare Data (if applicable): B. Flare type: Steam-assisted Air-assisted Non-assisted Other: Net heating value of combusted gas: 1200 Btu/scf 2. 3. Design exit velocity: 80 ft/sec Auto-ignitor Continuous Flame 4. System: 5. Is the presence of a flare pilot flame monitored? ⊠ Yes If yes, please describe the monitoring: Daily visual observation Is the auto-ignitor system monitored? ⊠ Yes No 6. If yes, please describe the monitoring: Electronic notification

EMISSION UNIT (Ref No.)	FEDERAL or STATE REGULATION  Ex. 40 CFR Part, Subpart Ex. 11 Miss. Admin. Code Pt. 2, R. 1.4.B(2).	CONSTRUCTION DATE	STARTUP DATE	REMOVAL DATE
Example: Engines	40 CFR 63, Subpart ZZZZ	10/01/2002	11/15/2019	N/A
Example: Fugitive Emissions	40 CFR 60, Subpart OOOOa	10/01/2019	11/15/2019	N/A
Example: Flare	11 Miss. Admin. Code Pt. 2, R.1.4.B(2).	12/01/2019	12/02/2019	N/A
This list of examination should be comp	mples is not intended to be conclusive for each type of emission source. Th oleted.	is list only provides e.	xamples of ho	w the table
AA-001 Flare and facility wide	11 Miss. Admin. Code Pt. 2, R.1.4.B(2).	01/18/2018	03/03/2023 (est.)	N/A
AA-003 Fugitive Emissions	40 CFR 60, Subpart OOOOa	01/18/2018	03/03/2023 (est.)	N/A
AA-003 Fugitive Emissions	40 CFR 60, Subpart OOOOa	01/18/2018	01/18/2018	N/A
AA-001 Flare and facility wide	11 Miss. Admin. Code Pt. 2, R.1.4.B(2).	01/18/2018	01/18/2018	N/A

MS Oil Production General Permit NOI, Section OPGP-G, v. 2019.1

## MDEQ NOTICE OF INTENT FOR COVERAGE UNDER THE OIL PRODUCTION GENERAL PERMIT TO CONSTRUCT/OPERATE AIR EMISSIONS EQUIPMENT AT A SYNTHETIC MINOR SOURCE

#### Compliance Plan **Section OPGP-G**

Part 2. Applicable Requirements

List all applicable state and federal requirements, including emission limits, operating restrictions, etc., and the applicable test methods or monitoring used to demonstrate compliance with each applicable requirement. Clearly identify federal regulations from state requirements. Provide the compliance status as of the day the application is signed.

EMISSION UNIT (Ref No.)	APPLICABLE REQUIREMENT (Specific Regulatory citation)	POLLUTANT	LIMITS/ REQUIREMENTS	TEST METHOD/ COMPLIANCE MONITORING
Example: Compressor	Item 8 of Table 2d of 40 CFR 63, Subpart ZZZZ	HAPs	Change oil and filter every 2,160 hours of operation or annually, whichever comes first; Inspect spark plugs every 2,160 hours of operation or annually, whichever comes first, and replace as necessary; and Inspect all hoses and belts every 2,160 hours of operation or annually, whichever comes first, and replace as necessary.	Monitoring of compressor hours of operation
Example: Tanks	40 CFR 60.5395(a)(2)	VOC and Methane	Must reduce VOC emissions by 95.0 percent within 60 days after startup of production.	Tank emissions are routed to the flare for destruction at all times of operations.
Example: Flare	11 Miss. Admin. Code Pt. 2, R.1.4.B(2).	H₂S	1 grain H <sub>2</sub> S per 100 standard cubic feet (1 gr/100 scf)	Recordkeeping of H2S composition of gas by gas analysis; Maintenance of continuous flame for gas combustion.
This list of example	les is not intended to be conclusive for each type of c	emission source. Thi	is list only provides examples of how the tai	ble should be completed.
AA-001, Flare & facility wide	1 Miss. Admin. Code Pt. 2, R.1.4.B(2).	H₂S	Any gas stream containing as much as 1 grain H <sub>2</sub> S per 100 standard cubic feet (1 gr/100 scf) must be incinerated prior to discharge to the atmosphere	Recordkeeping of H2S composition of gas by gas analysis; Maintenance of continuous flame for gas combustion.
AA-003 Fugitive Emissions	40 CFR 60.5365a(i)	VOC and Methane	Applicability	Applicability only
AA-003 Fugitive Emissions	40 CFR 60.5397a(a-g)	VOC and Methane	Develop a fugitive emission monitoring plan	Written Plan development

MS Oil Production General Permit NOI, Section OPGP-G, v. 2019.1

## MDEQ NOTICE OF INTENT FOR COVERAGE UNDER THE OIL PRODUCTION GENERAL PERMIT TO CONSTRUCT/OPERATE AIR EMISSIONS EQUIPMENT AT A SYNTHETIC MINOR SOURCE

### Compliance Plan Section OPGP-G

#### Part 2. Applicable Requirements

List all applicable state and federal requirements, including emission limits, operating restrictions, etc., and the applicable test methods or monitoring used to demonstrate compliance with each applicable requirement. Clearly identify federal regulations from state requirements. Provide the compliance status as of the day the application is signed.

EMISSION UNIT (Ref No.)	APPLICABLE REQUIREMENT (Specific Regulatory citation)	POLLUTANT	LIMITS/ REQUIREMENTS	TEST METHOD/ COMPLIANCE MONITORING
AA-003 Fugitive Emissions	40 CFR 60.5397a(h)	VOC and Methane	Fugitive emission source repair or replacement requirements	Recordkeeping of repair/replacement
AA-003 Fugitive Emissions	40 CFR 60.5425a and Table 3	VOC and Methane	Applicability of General Provisions of 40 CFR 60, Subpart A	Applicability only
AA-003 Fugitive Emissions	40 CFR 60.5410a(j)	VOC and Methane	Demonstration of initial compliance	Monitoring
AA-003 Fugitive Emissions	40 CFR 60.415a(h)	VOC and Methane	Demonstration of continuous compliance	Monitoring
AA-003 Fugitive Emissions	40 CFR 60.5420a(c)	VOC and Methane	Recordkeeping requirements	Monitoring and Recordkeeping
AA-003 Fugitive Emissions	40 CFR 60.5420a(b)	VOC and Methane	Reporting requirements	Reporting
AA-007 Storage Tanks	40 CFR 60.5365a(e)	VOC and Methane	Applicability determination may take into account legally and practically enforceable limit on tank emissions	Applicability Only. Federally enforceable limit requested for avoidance.

MS Oil Production General Permit NOI, Section OPGP-G, v. 2019.1

## MISSISSIPPI DEPARTMENT OF ENVIRONMENTAL OUALITY APPLICATION FOR AIR POLILITION CONTROL

		VIJ	MIDEQ			ATTOC		ERMIT		110	11 CO	.4116	JL
Tar	nk	Sum	mary	_							Sect	ion	H
			n Point Descripti										
	Note such	e: Secti 1 as in c	ons 3-7 below do not has report generated by L	ave to EPA's	be comp TANKS s	leted if all o software, an	of the requ ad attached	iired info d to the a	rmation is pplication.	provi	ded else	ewhere	2,
•	Α.	Emiss	ion Point Designation	(Ref. N	lo.):	_TK (	)1	<u>.</u>					-
	B.	Produ	ct(s) Stored: Crude C	Dil									-
(	C.	Status	: Operating		$\boxtimes$	Proposed			☐ Unde	r Con	structio	on	
	D.	Date of construction, reconstruction, or most recent modification (for existing sources) or date of anticipated construction:  09/2017											
2.	Tai	nk Da	ata						<u></u>				·
	A.	Tank :	Specifications:										
		2. 3. 4. 5.	Design capacity True vapor pressure at Maximum true vapor p Reid vapor pressure at Density of product at s Molecular weight of pr	ressure storage torage	e (as def e temper tempera	ined in §60. ature: ture:	.111b) _ -	21000 4.5 5 5 6.26 48.41	gallons psia @ psia @ psia @ psia @ lb/gal lb/lbmo	l	70 10 10	00	°F °F
	B.	Tank	Orientation:	] Ve	rtical			□ I	Horizontal				
•	C.	Туре	of Tank:										
			Fixed Roof		Externa	al Floating F	loof		Internal F	loatin	g Roof		
			Pressure		Variabl	le Vapor Spa	ace		Other:	_	_		
	D.		tank equipped with a V describe below and in					Yes		No	0		
	E.		st City: Jackson, MS		Merid	ian, MS		Tupelo,	MS		Mobil	e, AL	
			New Orleans, LA		Memp	his, TN		Baton R	louge, LA				!
	F.		EPA TANKS report inc Tanks software was use						☐ Yes	5		No	

FOR	MDEQ	1	MISSISSIPPI DEPARTMENT OF ENVIRONMENTAL QUALITY APPLICATION FOR AIR POLLUTION CONTROL PERMIT								
Tank	Sun	ımary	•							-	Section H
		ntal Fixed Roof T	ank								
A. B. C. D. E. F. G.	Shell Shell Work Maxi Is the Is the	Length: Diameter: cing Volume: mum Throughput: e tank heated? e tank underground? Color/Shade: Gray/Light			fe	al/yr		No No		Alumin Red/Pri	um/Diffuse mer
H.	Shell	Condition:	Good			] ]	Poor				
4. Ve	ertica	Fixed Roof Tan	k							-	
A.	Dime 1. 2. 3. 4. 5. 6. 7.	ensions: Shell Height: Shell Diameter: Maximum Liquid Heigh Average Liquid Heigh Working Volume: Turnovers per year: Maximum throughput: Is the tank heated?	t:	Yes	20 12 19 10 16,800 261.7 4396644	f	feet feet feet gal gal/y				
B.	<ol> <li>2.</li> </ol>	Characteristics: Shell Color/Shade: White/White Gray/Light Shell Condition: Characteristics:		Good	Aluminum Gray/Med	-		r		Alumin Red/Pri	um/Diffuse mer
	1.	Roof Color/Shade:  White/White  Gray/Light			Aluminum Gray/Med	•	cula	r		Aluminur Red/Prim	
	2.	Roof Condition:	$\boxtimes$	Good			]	Poor			
	3.	Туре:		Cone		Þ	3	Dome			
	4.	Height: 0.1		feet							

### MISSISSIPPI DEPARTMENT OF ENVIRONMENTAL FORM 5 MDF.O OUALITY APPLICATION FOR AIR POLLUTION CONTROL

_ `			MIDEQ	PERMIT	
Ta	ınk	Sun	ımary		Section H
5.			l Floating Roof Tai	nk	<u> </u>
	A.		Characteristics:		
		1.	Diameter:	feet	
		2.	Tank Volume:	gal	
		3.	Turnovers per year:		
		4.	Maximum Throughput:	gal/yr	
		5.	Number of Columns:		
		6.	Self-Supporting Roof?	☐ Yes ☐ No	
		7.	Effective Column Diame	<u> </u>	
			9"x7" Built-up Col		☐ Unknown
		8.	Internal Shell Condition:		T
		^	Light Rust		Lining
		9.	External Shell Color/Sha  White/White		num/Diffuse
			White/White	☐ Aluminum/specular ☐ Alumin	ium/Dinuse
			☐ Gray/Light	☐ Gray/Medium ☐ Red/Pr	imer
		10.	External Shell Condition	: Good Poor	
		11.	Roof Color/Shade:		
			☐ White/White	☐ Aluminum/Specular ☐ Aluminum/Di	ffuse
			☐ Gray/Light	☐ Gray/Medium ☐ Red/Primer	
		12.	Roof Condition:	☐ Good ☐ Poor	
	B.	Rim	Seal System:		
		1.		Mechanical Shoe	Vapor-mounted
		2.	Secondary Seal:	Shoe-mounted	☐ None
	C.	Deck	Characteristics:		
		1.	Deck Type:	Bolted	
		2.	Deck Fitting Category:	☐ Typical ☐ Detail	
6.	Ex	terna	d Floating Roof Ta	nk	
	Α.	Tank	Characteristics		
	1	1.	Diameter:	feet	
		2.	Tank Volume:	gal	
		3.	Turnovers per year:		
		4.	Maximum Throughput:	gal/yr	
		5.	Internal Shell Condition:		
			☐ Light Rust	☐ Dense Rust ☐ Gunite Lini	ng

### MISSISSIPPI DEPARTMENT OF ENVIRONMENTAL FORM 5 MDF. OUALITY APPLICATION FOR AIR POLLUTION CONTROL

			147	DEQ		PERMIT							
Ta	nk	Sum	mar	y							·		Section H
6.	Ex	terna	l Floa	ating Roof	Tank	(cı	ontinued)						
	A.		Paint C	teristics (cont Color/Shade: Vhite/White	inued):	]	Aluminum/Sp	ecular			Aluminum	/Diff	use
			□ G	iray/Light			Gray/Medium				Red/Prime	r	
		7.	Paint C	Condition:		]	Good			Poor			
	B. Roof Characteristics 1. Roof Type:												
		2.	Roof F	itting Categor	ry:			Typic	al		☐ Detail		
	C.			uction and Riz Construction:	m-Seal S	Syst	em:	Weld	ed		☐ Rivete	d	
	2. Primary Seal:  ☐ Mechanical Shoe ☐ Liquid-mounted ☐ Vapor-mounted												
		3.		lary Seal None	] Shoe	e-mo	ounted		Rim-r	nounte	ed 🗆	l v	Veather shield
<u>7.</u>	Po	llutar	ıt Em	issions									
	A.	Fixed Pollu		Emissions:	Worl	cing	Loss (tons/yr)		Breathi	ng Los	s (tons/yr)	Tot	al Emissions
		VOC											(tons/yr) 70.58
		Hexa	ne	_									3.1734
		Benze				_							0.2790
			benzene	e									0.0169
		Tolue									_		0.3889
		Xyler	1e	<u>i</u> _	-								0.2029
_	B.	Floati	ing Roo	of Emissions:									
	Pollutant <sup>1</sup> Rim Seal Loss (tons/yr)			Loss	Withda Los (tons	SS	l Deck Fitt Loss (tons/y)		Deck S Los (tons/	s	Landing Lo (tons/yr)		Total Emissions (tons/yr)
ľ													
	<ol> <li>All regulated air pollutants including hazardous air pollutants emitted from this source should be listed in accordance with the Permit Application Instructions. A list of regulated air pollutants and hazardous air pollutants is provided in the Application Instructions.</li> <li>Landing losses should be determined according to the procedures in <i>Organic Liquid Storage Tanks</i> chapter of EPA's AP-42 emission factors. If the roof is not landed at least once/yr, enter "NA".</li> </ol>												

## MISSISSIPPI DEPARTMENT OF ENVIRONMENTAL FORM 5 MDEO QUALITY APPLICATION FOR AIR POLLUTION CONTROL

		PERMIT
Ta	nk	Summary Section H
1.	En	ission Point Description
		: Sections 3-7 below do not have to be completed if all of the required information is provided elsewhere, as in a report generated by EPA's TANKS software, and attached to the application.
	A.	Emission Point Designation (Ref. No.): TK-02, TK-03
	B.	Product(s) Stored: Crude Oil
	C.	Status:    Operating    Proposed    Under Construction
	D.	Date of construction, reconstruction, or most recent modification (for existing sources) or date of anticipated construction:  09/2017
2.	Ta	nk Data
	A.	Tank Specifications:
		1. Design capacity 2. True vapor pressure at storage temperature: 3. Maximum true vapor pressure (as defined in §60.111b) 4. Reid vapor pressure at storage temperature: 5. Density of product at storage temperature: 6. Molecular weight of product vapor at storage temp.  16,800 psia @ 70 PF  12.0 psia @ 100 PF  11.7 psia @ 100 PF  46.63 Ib/Ibmol
	B.	Tank Orientation:   Vertical   Horizontal
	C.	Type of Tank:
		☐ Fixed Roof ☐ External Floating Roof ☐ Internal Floating Roof
		☐ Pressure ☐ Variable Vapor Space ☐ Other:
	D.	Is the tank equipped with a Vapor Recovery System?  Yes  No  If yes, describe below and include the efficiency. ———
	E.	Closest City:     Jackson, MS
		☐ New Orleans, LA ☐ Memphis, TN ☐ Baton Rouge, LA
	F.	Is an EPA TANKS report included for this tank in the application?

FORM 5 MDEQ			MISSISSIPPI DEPARTMENT OF ENVIRONMENTAL QUALITY APPLICATION FOR AIR POLLUTION CONTROL PERMIT							
Ta	nk	Sun	nmary							Section H
3.	Ho	rizoı	ntal Fixed Roof Ta	ank		· · · · · · · · · · · · · · · · · · ·				
	A. B. C. D. E. F.	Shell Work Maxi Is the	Length: Diameter: king Volume: imum Throughput: e tank heated? e tank underground? Color/Shade:		Yes Yes	feet feet gal gal minum/Specul	t /yr 	No No		Aluminum/Diffuse
		П	Gray/Light	Г	Grav	/Medium				Red/Primer
	Н.	Shell	Condition:	Good	•		Poor	r		Acco i inno
4.	Ve	rtica	l Fixed Roof Tank							
	A.	Dime 1. 2. 3. 4. 5. 6. 7.	ensions: Shell Height: Shell Diameter: Maximum Liquid Height Average Liquid Height Working Volume: Turnovers per year: Maximum throughput: Is the tank heated?		Yes	20 12 19 10 16,800 261.7 4396644	feet fcct feet feet gal gal/y			
	B.	Shell 1. 2.	Characteristics: Shell Color/Shade: ☐ White/White ☐ Gray/Light Shell Condition:	$\boxtimes$	□ □ Good	Aluminum/S	•	ır		Aluminum/Diffuse Red/Primer
	C.	Roof 1.	Characteristics: Roof Color/Shade: White/White Gray/Light			Aluminum/S	_	ır		Aluminum/Diffuse Red/Primer
		2.	<b>Roof Condition:</b>	$\boxtimes$	Good			Poor		
		3.	Туре:		Cone		$\boxtimes$	Dome		
		4.	Height: 0.1		feet					

### MISSISSIPPI DEPARTMENT OF ENVIRONMENTAL FORM 5 MDEO QUALITY APPLICATION FOR AIR POLLUTION CONTROL

			3226	PERMIT	
Ta	ınk	Sun	ımary		Section H
5.	Int	erna	l Floating Roof Tan	k	·
	Α.		Characteristics:		
		1.	Diameter:	feet	
		2.	Tank Volume:	gal	
		3.	Turnovers per year:	<del></del>	
		4.	Maximum Throughput:	gal/yr	
		5.	Number of Columns:		
		6. 7.	Self-Supporting Roof? Effective Column Diameter	Yes No	
		7.	9"x7" Built-up Colum		Unknown
		8.	Internal Shell Condition:		
			☐ Light Rust	☐ Dense Rust ☐ Gunite	Lining
		9.	External Shell Color/Shad		J
			☐ White/White	☐ Aluminum/Specular ☐ Alumin	um/Diffuse
			☐ Gray/Light	☐ Gray/Medium ☐ Red/Pri	mer
		10.	External Shell Condition:	☐ Good ☐ Poor	
		10.	Roof Color/Shade:		
		11.	White/White	☐ Aluminum/Specular ☐ Aluminum/Diff	fuse
			☐ Gray/Light	☐ Gray/Medium ☐ Red/Primer	
		12.	<b>Roof Condition:</b>	☐ Good ☐ Poor	
	B.	Rim 1.	Seal System: Primary Seal:   Me	echanical Shoe	Vapor-mounted
		2.	Secondary Seal:	Shoe-mounted	None
	C.	Deck	Characteristics: Deck Type:	Bolted	
		2.	Deck Fitting Category:	☐ Typical ☐ Detail	
6.	Ex	terna	l Floating Roof Tan	k	
	Α.	lank	Characteristics Diameter:	feet	
		1. 2.	Tank Volume:	gal	
		2. 3.	Turnovers per year:	gai	
		3. 4.	Maximum Throughput:	gal/yr	
		5.	Internal Shell Condition:	gan J.	
		٥.	Light Rust	☐ Dense Rust ☐ Gunite Linin	g

#### MISSISSIPPI DEPARTMENT OF ENVIRONMENTAL FORM 5 | MDEQ **QUALITY APPLICATION FOR AIR POLLUTION CONTROL PERMIT Tank Summary** Section H 6. External Floating Roof Tank (continued) Tank Characteristics (continued): Paint Color/Shade: White/White Aluminum/Specular Aluminum/Diffuse Red/Primer Gray/Light Gray/Medium 7. ☐ Good Paint Condition: ☐ Poor **Roof Characteristics** Double Deck Pontoon Roof Type: 2. Roof Fitting Category: **Typical** Detail Tank Construction and Rim-Seal System: Tank Construction: Welded Riveted 2. Primary Seal: Vapor-mounted Mechanical Shoe Liquid-mounted Secondary Seal 3. Weather shield None Rim-mounted Shoe-mounted **Pollutant Emissions Fixed Roof Emissions:** Pollutant<sup>1</sup> **Total Emissions** Breathing Loss (tons/yr) Working Loss (tons/yr) (tons/yr) VOC All tank emissions included in TK-01 Hexane Benzene Ethylbenzene Toluene

B. Floating Roof Emissions:

**Xylene** 

Pollutant <sup>1</sup>	Rim Seal Loss	Withdrawal Loss	Deck Fitting Loss	Deck Seam Loss	Landing Loss <sup>2</sup> (tons/yr)	Total Emissions
	(tons/yr)	(tons/yr)	(tons/yr)	(tons/yr)		(tons/yr)
		-				

<sup>1.</sup> All regulated air pollutants including hazardous air pollutants emitted from this source should be listed in accordance with the Permit Application Instructions. A list of regulated air pollutants and hazardous air pollutants is provided in the Application Instructions.

<sup>2.</sup> Landing losses should be determined according to the procedures in *Organic Liquid Storage Tanks* chapter of EPA's AP-42 emission factors. If the roof is not landed at least once/yr, enter "NA".

### MISSISSIPPI DEPARTMENT OF ENVIRONMENTAL FORM 5 MDEO QUALITY APPLICATION FOR AIR POLLUTION CONTROL

		PERMIT	
Ta	nk	Summary	Section H
1.	En	mission Point Description	
	Note such	te: Sections 3-7 below do not have to be completed if all of the required information is provi ch as in a report generated by EPA's TANKS software, and attached to the application.	ided elsewhere,
	A.	Emission Point Designation (Ref. No.): TK-04	
	B.	Product(s) Stored: Produced Water	
	C.	Status:	nstruction
	D.	Date of construction, reconstruction, or most recent modification (for existing sources) or date of anticipated construction:  09/2017	
2.	Ta	ank Data	
	A.	Tank Specifications:	
		1. Design capacity	_
		2. True vapor pressure at storage temperature: 0.106 psia @	70 °F °F
		<ul> <li>Maximum true vapor pressure (as defined in §60.111b)</li></ul>	82 °F °F
		5. Density of product at storage temperature:  8.2 lb/gal	
		6. Molecular weight of product vapor at storage temp. 46.63 lb/lbmol	
	B.	Tank Orientation:	
	C.	Type of Tank:	
		☐ Fixed Roof ☐ External Floating Roof ☐ Internal Floating	ng Roof
		☐ Pressure ☐ Variable Vapor Space ☐ Other:	·
	D.	Is the tank equipped with a Vapor Recovery System?  Yes N  If yes, describe below and include the efficiency.	0
	E.	Closest City:  Solution	Mobile, AL
		☐ New Orleans, LA ☐ Memphis, TN ☐ Baton Rouge, LA	, 110
	F.	Is an EPA TANKS report included for this tank in the application?	⊠ No
	-		

#### MISSISSIPPI DEPARTMENT OF ENVIRONMENTAL **MDEQ** FORM 5 QUALITY APPLICATION FOR AIR POLLUTION CONTROL **PERMIT Tank Summary Section H Horizontal Fixed Roof Tank** Shell Length: Shell Diameter: feet B. Working Volume: C. gal Maximum Throughput: gal/yr E. Yes Is the tank heated? No F. Is the tank underground? Yes No Shell Color/Shade: Aluminum/Diffuse Aluminum/Specular Red/Primer Gray/Light Gray/Medium Shell Condition: Good Poor **Vertical Fixed Roof Tank Dimensions:** Shell Height: 1. 20 feet 2. Shell Diameter: 12 feet 3. Maximum Liquid Height: feet 4. Average Liquid Height: 10 feet 5. Working Volume: 16,800 gal 6. Turnovers per year: 261.7 7. Maximum throughput: 4396644 gal/yr 8. Is the tank heated? Yes No **Shell Characteristics:** В. Shell Color/Shade: White/White Aluminum/Specular Aluminum/Diffuse Gray/Light Gray/Medium Red/Primer 2. Shell Condition: 冈 Good **Poor Roof Characteristics:** Roof Color/Shade: White/White Aluminum/Specular Aluminum/Diffuse $\boxtimes$ Gray/Light Gray/Medium Red/Primer

 $\square$ 

0.1

Good

Cone

feet

**Poor** 

Dome

M

**Roof Condition:** 

Type:

Height:

2.

3.

4.

|--|

## MISSISSIPPI DEPARTMENT OF ENVIRONMENTAL QUALITY APPLICATION FOR AIR POLLUTION CONTROL PERMIT

		_	1111111	_	PERMIT						
Tank Summary						Section H					
5. Internal Floating Roof Tank											
	A.		Characteristics:								
		1.	Diameter:		feet						
		2.	Tank Volume:		gal						
		3.	Turnovers per year:		<del></del>						
		4.	Maximum Throughput:		gal/yr						
		5.	Number of Columns:		——————————————————————————————————————						
		6.	Self-Supporting Roof?		☐ Yes ☐ No						
		7.	Effective Column Diame		O" Diameter Bine	Unknown					
		8.	9"x7" Built-up Col Internal Shell Condition:		8" Diameter Pipe	LI Ulikilowii					
		0.	Light Rust		☐ Dense Rust ☐ Gunite	I ining					
		9.	External Shell Color/Sha	de:	_ Sunte	Liming					
			☐ White/White		Aluminum/Specular	um/Diffuse					
					•						
			☐ Gray/Light		Gray/Medium Red/Pri	mer					
		10.	External Shell Condition	:	☐ Good ☐ Poor						
		11.	Roof Color/Shade:								
			☐ White/White		Aluminum/Specular	fuse					
			☐ Gray/Light		Gray/Medium						
				_							
		12.	<b>Roof Condition:</b>		Good Poor						
	B.	Dim	Seal System:								
	D.	1.									
			i i i i i i i i i i i i i i i i i i i		_ ·	_					
		2.	Secondary Seal:	Sho	e-mounted	☐ None					
	C.	Deck	Characteristics:								
		1.	Deck Type:	Bol	ted						
		_	D 1 D 1								
		2.	Deck Fitting Category:		☐ Typical ☐ Detail						
6.	Ex	ternal Floating Roof Tank									
	Α.	Tank Characteristics									
	A.	1 ank	Diameter:		feet						
		2.	Tank Volume:		gal						
		3.	Turnovers per year:		ga						
		4.	Maximum Throughput:		gal/yr						
		5.	Internal Shell Condition:		<i>G y</i>						
			☐ Light Rust		☐ Dense Rust ☐ Gunite Linin	g					
			-			_					

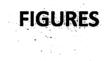
#### MISSISSIPPI DEPARTMENT OF ENVIRONMENTAL FORM 5 | MDEO **QUALITY APPLICATION FOR AIR POLLUTION CONTROL PERMIT Tank Summary Section H External Floating Roof Tank (continued)** Tank Characteristics (continued): Paint Color/Shade: White/White Aluminum/Specular Aluminum/Diffuse Gray/Light Gray/Medium Red/Primer 7. Paint Condition: ☐ Good ☐ Poor **Roof Characteristics** Roof Type: Pontoon Double Deck 2. Roof Fitting Category: **Typical** Detail Tank Construction and Rim-Seal System: Tank Construction: Welded Riveted 2. Primary Seal: Mechanical Shoe Liquid-mounted Vapor-mounted 3. Secondary Seal None Shoe-mounted Rim-mounted П Weather shield **Pollutant Emissions Fixed Roof Emissions:** Pollutant<sup>1</sup> **Total Emissions** Working Loss (tons/yr) Breathing Loss (tons/yr) (tons/yr) VOC 0.7058 Hexane 0.0332 Benzene 0.0028 Ethylbenzene 0.0002 Toluene 0.0039 Xvlene 0.0020

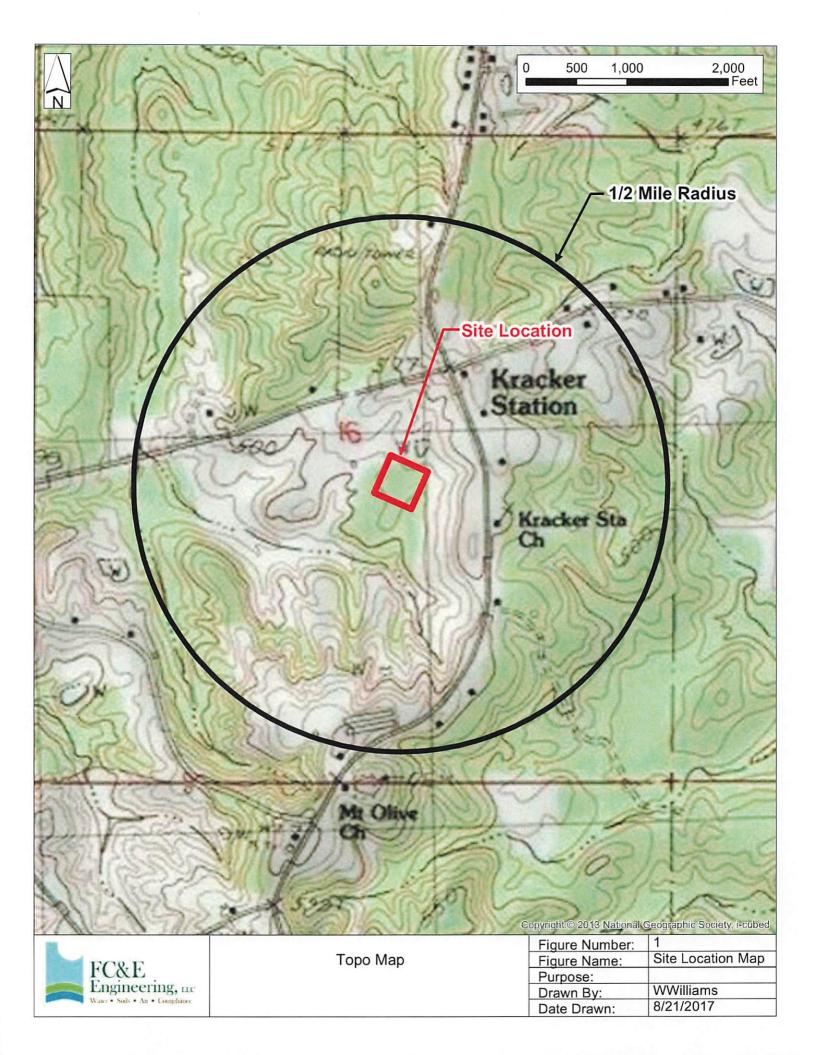
B. Floating Roof Emissions:

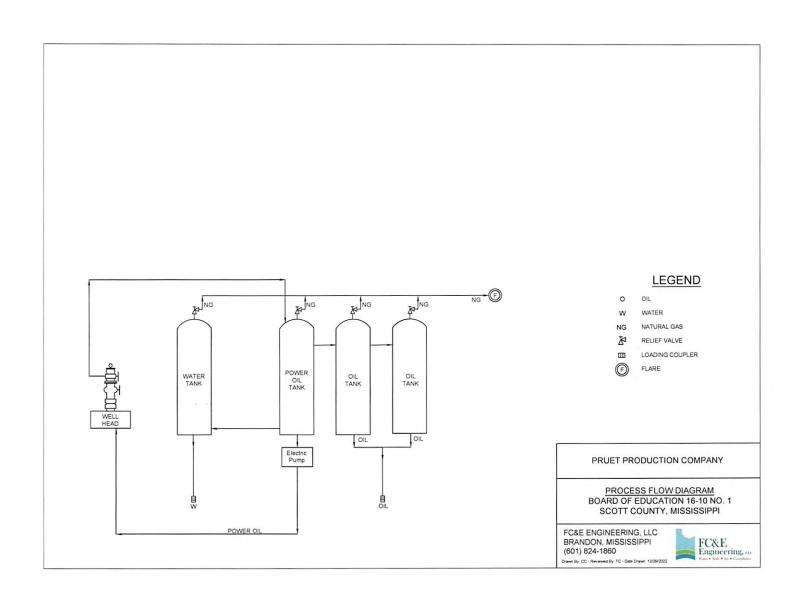
Pollutant <sup>1</sup>	Rim Seal	Withdrawal	Deck Fitting	Deck Seam	Landing Loss <sup>2</sup>	Total Emissions
	Loss (tons/yr)	Loss (tons/yr)	Loss (tons/yr)	Loss (tons/yr)	(tons/yr)	(tons/yr)

<sup>1.</sup> All regulated air pollutants including hazardous air pollutants emitted from this source should be listed in accordance with the Permit Application Instructions. A list of regulated air pollutants and hazardous air pollutants is provided in the Application Instructions.

<sup>2.</sup> Landing losses should be determined according to the procedures in *Organic Liquid Storage Tanks* chapter of EPA's AP-42 emission factors. If the roof is not landed at least once/yr, enter "NA".







#### **ATTACHMENT A**

Calculations for Pruet Board of Education 16-10 No. 1 Tank Battery

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#### **Site Information for Calculations**

Site Name: Board of Education 16-10 No. 1 Tank Battery

Potential Crude Production 24,000 bbl/yr
Potential Gas production 21,900 mcf/yr
Potential Produced Water 1,000 bbl/yr

Initial Crude Production 66 bbl/day (expected maximum daily production)
Initial Gas Production 60 mcf/day (expected maximum daily production)
Initial Water Production 1 bbl/day (expected maximum daily production)

Crude Gravity 49

Oil tank W&B Losses

Oil tank Flash Gas

1.31 SCF/stock tank bbl (estimated using E&P Tanks)

Oil tank Flash Gas

26.3 SCF/stock tank bbl (estimated using E&P Tanks)

Water tank W&B Losses

O.0131 SCF/stock tank bbl (using 1% of oil tank emissions)

Water tankFlash Gas

O.263 SCF/stock tank bbl (using 1% of oil tank emissions)

VRU recovery efficiency 0.00% Flare destruction efficiency 98.00%

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### **Emission Point Summary**

Emission Point Number	Emission Point Description	Design Capacity	Units	Operating Hours	
AA-001	Flare	10.25	MMBtu/hr	8760	
AA-001a	-001a Flare Pilot		MMBtu/hr	8760	
AA-003	A-003 Fugitive emissions- equipment leaks		-	8760	
AA-005	Misc. Chemical Tanks	2	-	8760	
AA-006 Oil and Water Storage Tanks		ä		8760	
AA-007	Truck Loading	16,000	gal/hr	As needed	

Note: Storage tanks vent to the flare.

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### **Proposed Annual Emissions, controlled**

Emission	Balling Carrier and Carrier	Annual Emissions, tpy						GHG/Emissions; tpy					
Unit (D)	<u>Emission</u> /Unit	PM.	PM10	PM2.5	VOC	NOX	CO	SO2'	Total HAPs	©02	CH4	N20	(CO20)
AA-001	Flare	0.03	0.03	0.03	4.81	1.06	4.84	41.14	0.2415	1907.95	5.73	0.00	2052.02
AA-001a	Flare Pilot	0.00	0.00	0.00	0.00	0.02	0.02	0.00	0.0004	25.59	0.00	0.00	25.62
AA-003	Fugitive emissions- equipment leaks	-	-	-	0.33	-	-		0.0228	0.02	0.25	0.00	6.23
AA-005	Misc. Chemical Tanks (4)	-	-	-	0.02	-	-	•	0.0190	-	-	-	•
AA-006	Oil and Water Tanks (4)		Gas routed to flare										
AA-007	Truck Loading				3.67				0.1644	0.01	0.05	0	1.37
	Totals	0.03	0.03	[10.03]	8.84	1:08	4.86	41:14	0.4480	1933.58	6,03	10,00	2085;24

### Notes:

Storage tanks emissions are included in flare emissions.

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### Potential Annual Emissions, uncontrolled

Funtantan		Annual Emissions, tpy						GHG Emissions, tpy					
Emission Unit ID	Emission Unit	PM	PM10	PM2.5	voc	NOx	со	SO2	Total HAPs	CO2	CH4	N2O	CO2e
AA-001	Facility gas emissions	-		-	240.62	-			12.07	94.82	69.49	0.00	1832.17
AA-003	Fugitive emissions- equipment leaks	-	-		0.33				0.02	0.02	0.25	0.00	6.23
AA-005	Misc. Chemical Tanks	-	-	-	0.02	-	-	-	0.02	-			-
AA-006	Oil and Water Storage Tanks		Gas	routed to	flare								
AA-007	Truck Loading				3.67				0.1644	0.01	0.05	0	1.37
	Totals	0.00	0.00	0.00	244.64	0.00	0.00	0.00	12.28	94.85	69.80	0.00	1839.77

Notes:

Storage tanks emissions are included in flare emissions, AA-001.

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### Facility Maximum Hourly Emissions, Controlled

Footseles		Emissions, lb/hr								GHG Emissions, lb/hr			
Emission Unit ID	Emission Unit	PM	PM10	PM2.5	voc	NOx	со	SO2	Total HAPs	CO2	CH4	N2O	CO2e
AA-001	Flare	0.01	0.01	0.01	1.10	0.24	1.11	9.39	0.06	435.61	1.31	0.00	468.50
AA-001a	Flare Pilot	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	5.84	0.00	0.00	5.85
AA-003	Fugitive emissions- equipment leaks	-		-	0.08	18		-	0.01	0.00	0.06	0.00	1.42
AA-005	Misc. Chemical Tanks	-	-	-	0.00	-	-	-	0.00	-			0.00
AA-006	Oil and Water Storage Tanks				GAS ROU	TED TO FL	ARE						
AA-007	Truck Loading	-	-	-	117.72	-	-	-	5.27	0.00	0.01	(	0.31
	Totals	0.01	0.01	0.01	118.90	0.25	1.11	9.393	5.33	441.46	1.38	0.00	476.08

Notes:

Storage tanks emissions are included in flare emissions.

Truck loading hourly emissions are dictated by the capacity of the transfer pump

4.38 tpy = 1 PPH

### **Flash Gas Analysis and Conversions**

Component	VOC and/or HAP?	Mol %	Wt %
Total S	None	***	0.00000%
CO2	None	0.362%	0.160%
N2	None	0.000%	0.000%
Methane	None	11.546%	1.852%
Ethane	None	6.480%	1.949%
Propane	VOC	19.755%	8.712%
Isobutane	VOC	20.171%	11.724%
Butane	VOC	12.576%	7.309%
Isopentane	VOC	9.194%	6.633%
Pentane	VOC	5.953%	4.295%
Hexane	VOC	3.906%	3.366%
Heptanes	VOC	6.630%	6.644%
Benzene	VOC and HAP	0.390%	0.544%
Toluene	VOC and HAP	0.388%	0.639%
e-Benzene	VOC and HAP	0.015%	0.028%
Xylenes	VOC and HAP	0.211%	0.400%
n-hexane	VOC and HAP	2.422%	3.726%
Total VOC		79.190%	54.020%
Total HAP		3.426%	5.337%

Heat of combustion, Btu/ft <sup>3</sup>	2465.9
Molecular weight	46.02

Gas analysis generated by E&P Tanks software.

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### **Produced Gas Analysis and Conversions**

		,		
Component	VOC and/or HAP?	Mol %	Wt %	
Total S	None	0.000%	2.72600%	
CO2	None	1.621%	12.544%	
N2	None	11.721%	37.729%	
Methane	None	61.556%	9.104%	
Ethane	None	7.925%	11.705%	
Propane	VOC	6.948%	5.338%	
Isobutane	VOC	2.404%	8.518%	
Butane	VOC	3.836%	3.592%	
Isopentane	VOC	1.303%	3.062%	
Pentane	voc	1.111%	1.640%	
Hexane	voc	0.500%	1.042%	
n-Hexane	VOC and HAP	0.312%	2.619%	
Heptanes+	voc	0.654%	0.109%	
Benzene	VOC and HAP	0.037%	0.121%	
Toluene	VOC and HAP	0.034%	0.020%	
e-Benzene	VOC and HAP	0.005%	0.131%	
Xylenes	VOC and HAP	0.033%	0.020%	
Total VOC		17.177%	28.918%	
Total HAP		0.421%	2.911%	

Heat of combustion, Btu/ft <sup>3</sup>	1353.0
Molecular weight	26.18

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**TANK W & B GAS COMPOSITION** 

Component	VOC and/or HAP?	Mol %	Wt %			
Total S	None	0.000%	0.00000%			
CO2	None	0.32%	0.25%	44.1	0.140414	
N2	None	0.00%	0.00%	28.01	0	
Methane	None	4.76%	1.35%	16.04	0.762878	
Ethane	None	7.23%	3.86%	30.07	2.174783	
Propane	VOC	24.31%	19.03%	44.1	10.72005	
Isobutane	VOC	23.60%	24.34%	58.12	13.71649	
Butane	VOC	14.17%	14.62%	58.12	8.235546	
Isopentane	VOC	9.38%	12.01%	72.15	6.766083	
Pentane	VOC	5.77%	7.39%	72.15	4.163055	
Hexane	VOC	3.28%	5.02%	86.18	2.8286	
Heptanes+	VOC	4.52%	8.03%	100.21	4.526586	
Benzene	VOC and HAP	0.32%	0.44%	78.11	0.247531	0.164355
Toluene	VOC and HAP	0.27%	0.44%	92.14	0.245092	
e-Benzene	VOC and HAP	0.01%	0.02%	106.17	0.009449	
Xylenes	VOC and HAP	0.12%	0.23%	106.16	0.129091	
n-hexane		1.95%	2.98%	86.18	1.677235	
Total VOC		85.75%	91.56%		56.34289	
Total HAP		2.660%	4.10%			

Heat of combustion, Btu/ft<sup>3</sup> 2796.8 Molecular weight 51.43

Note: W&B vapors and truck loading vapors assumed to have same composition Gas analysis generated by E&P Tanks software.

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### **Tank Uncontrolled Emissions Summary**

	Datamtial		Initial	
	<u>Potential</u>		<u>Production</u>	
Total flash gas ,	631,463	SCF/yr	72	SCF/hr
Total flash gas ,	37.52	tpy	8.56	lb/hr
Total tank W&B loss	31,453	SCF/yr	4	SCF/hr
Total tank W &B losses	2.09	tpy	0.48	lb/hr
Total tank emissions	39.60	tpy	9.04	lb/hr
Tank emissions to flare	39.60	tpy	9.04	lb/hr
	263.00			
	0.02	0.01	0.0000	
A. B. A.				

### Notes:

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<sup>1.</sup> Total flash gas calculated using gas/oil ratio from E&P tanks program and potential crude and water production

<sup>2.</sup> All tank emissions included with flare, Emission Point AA-001.

### Calculation of Criteria and Hazardous Flare Emissions Using 30-day Average Production Values

#### Gas Flow to Flare:

		<b>Potential</b>
Flow to flare of tank flash gas	=	37.52 tpy
Flow to flare of tank W&B emissions		2.09 tpy
flow to flare from truck loading	=	0.00 tpy
Total process gas to flare	=	39.60 tpy
Produced gas to flare	=	755.39 tpy
	=	21900.00 mcf/yr
Produced gas combustion heat	=	29630.70 MMBtu/yr
process gas combustion heat	=	1610.70 MMBtu/yr
flare gas combustion heat, total	=	31241.40 MMBtu/yr

			Potentia	Potential Emissions			
	<u>Pollutant</u>	Emission factor, Ibs/MMBtu	<u>lb/hr</u>	tpy	Pollutant	<u>lb/hr</u>	tpy
	NOx	0.068	0.243	1.062	n-hexane	0.0422	0.1848
Calculation	CO	0.31	1.106	4.842	benzene	0.0051	0.0225
	PM	0.00186	0.000	0.029	e-benzene	0.0046	0.0200
	VOC	mass balance	1.099	4.812	toluene	0.0018	0.0080
	SO <sub>2</sub>	mass balance	9.393	41.143	xylenes	0.0014	0.0061
P	M10/PM2.5	0.00745	0.027	0.116	Total HAPs	0.0551	0.2415

### Notes:

- 1. Emission factors from AP-42, Table 13.5-1, are used to calculate NOx and CO emissions, and PM emission factor from AP-42, Table 1.4-2.
- Mass balance calculations utilize flare input gas flow and a flare destruction efficiency of 98% minimum.
- 3. Mass balance for sulfur assumes all sulfur converted to SO2 in flare.

 ${\tt ink}$  Battery HAP emissions calculated using mass balance and 98% destruction efficiency Oil General Permit Coverage Application

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### Calculation of Maximum Hourly Criteria and Hazardous Flare Emissions Using Initial Production Values

### Gas Flow to Flare:

		<u>Potential</u>
Flow to flare of tank flash gas	=	8.56 lbs/hr
Flow to flare of tank W&B emissions		0.48 lbs/hr
flow to flare from truck loading	=	0.00 lbs/hr
Total process gas to flare	=	9.04 lbs/hr
Produced gas to flare	=	172.46 lbs/hr
	:	2.50 mcf/hr
Produced gas combustion heat	=	3.38 MMBtu/hr
process gas combustion heat	=	0.18 MMBtu/hr
flare gas combustion heat, total	=	3.57 MMBtu/hr

			Maximum Hourly Emissions			
	<u>Pollutant</u>	Emission factor, lbs/MMBtu	<u>lb/hr</u>	<u>Pollutant</u>	lb/hr	
	NOx	0.068	0.243	n-hexane	0.0422	
Calculation	n CO	0.37	1.320	benzene	0.0051	
	PM	0.00745	0.027	e-benzene	0.0046	
	VOC	mass balance	1.099	toluene	0.0018	
	SO <sub>2</sub>	mass balance	9.393	xylenes	0.0014	
				Total HAPs	0.0551	

#### Notes:

- 1. Emission factors from AP-42, Table 13.5-1, are used to calculate NOx and CO emissions, and PM emission factor from AP-42, Table 1.4-2.
- 2. Mass balance calculations utilize flare input process gas flow and a flare destruction efficiency of 98% minimum.
- 3. Mass balance for sulfur assumes all sulfur converted to SO2 in flare.
- 4. HAP emissions calculated using mass balance and 98% destruction efficiency

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### **Calculation of Uncontrolled Emissions of Produced Gas**

		<u>Potential</u>
Flow to flare from tank flash gas	=	37.52 tpy
Flow to flare from tank W&B emissions	=	2.09
flow to flare from truck loading	=	0.00 tpy
Produced gas to flare from power oil tank	=	755.39 tov

		<u>Potential</u>	<u>Emissions</u>
<u>Pollutant</u>	Emission factor, lbs/MMBtu	<u>lb/hr</u>	tpy
VOC	mass balance	54.937	240.62
H2S	mass balance	4.995	21.88
n-hexane	mass balance	2.109	9.24
benzene	mass balance	0.257	1.13
e-benzene	mass balance	0.228	1.00
toluene	mass balance	0.091	0.40
Calculation xylenes	mass balance	0.070	0.31
total HAPs	mass balance	2.756	12.07
methane	mass balance	15.866	69.49
CO2	mass balance	21.649	94.82

Note: For calculation of uncontrolled emissions, flare efficiency is 0%.

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### **Calculation of Flare GHG Emissions**

Process gas to flare, mmcf/yr 0.65
N2O emission factor, kg/mmBtu 0.0001
HHV, mmBtu/scf 0.001235
CO2 density, kg/ft3 0.052600
CH4 density, kg/ft3 0.019200
flare efficiency 98.00%

### **PROCESS GAS**

carbon	CO2 (from c	combustion)	CO2 input	CH4, uncombusted		N2O	CO2e
atoms	cubic ft.	tpy	tpy	cubic ft. tpy1		tpy <sup>1</sup>	tpy
			1.37E-01	1.51E+03	3.19E-02	8.87E-05	9.60E-01
1	7.39E+04	4.28E+00	*				4.28E+00
2	8.30E+04	4.80E+00					4.80E+00
3	3.79E+05	2.19E+01					2.19E+01
4	8.39E+05	4.85E+01		ĺ			4.85E+01
5+	8.54E+05	4.94E+01					4.94E+01
Total	2.23E+06	1.29E+02	1.37E-01	1.51E+03	3.19E-02	8.87E-05	1.30E+02

### **PRODUCED GAS**

produced gas to flare, mmcf/yr

21.90

carbon	CO2 (from combustion)		CO2 input	CH4, uncombusted		N2O	CO2e
atoms	cubic ft.	tpy	tpy	cubic ft.	cubic ft. tpy		tpy
			2.05E+01	2.70E+05	5.69E+00	2.98E-03	1.64E+02
1	1.32E+07	7.64E+02					7.64E+02
2	3.40E+06	1.97E+02					1.97E+02
3	4.47E+06	2.59E+02					2.59E+02
4	5.36E+06	3.10E+02					3.10E+02
5+	3.95E+06	2.28E+02				i	2.28E+02
Total	3.04E+07	1.76E+03	2.05E+01	2.70E+05	5.69E+00	2.98E-03	1.92E+03

Note: GHG emissions calculated using procedures from 40 CFR 98.233(n)(4)

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### **Equipment Component Fugitive Emissions**

Components	Counts	Emission Factor <sup>1</sup>	Emissions	Wt. Fraction	VOC Em	issions	VOC%	HAP Em	issions	GHG I	missions, t	on/yr
		scf/hr/component	lbs/hr	voc	lb/hr	tpy	HAP <sup>3</sup>	lb/hr	tpy	CO2	CH4	CO2e
Valves:	5											
gas/vapor	24	0.027	0.044702609	0.29	0.013	0.06	2.91%	0.001	0.006	0.005326	0.073798	1.85
light oil <sup>2</sup>	13	0.05	0.04484058	0.54	0.024	0.11	5.34%	0.002	0.010	0.005342	0.067296	1.69
heavy oil	0	0.0005	0	0.29	0.000	0.00	2.91%	0.000	0.000	0	0	0.00
Pumps:			0	0.29			2.91%	0.000	0.000	0	0	0.00
Light oil	0	0.01	0	0.73	0.000	0.00	1.66%	0.000	0.000	0	0	0.00
heavy oil	0	0	0	0.29			2.91%	0.000	0.000	0	0	0.00
Flanges:	10		0	0.29			2.91%	0.000	0.000	0	0	0.00
gas/vapor		0	0	0.29	0.000	0.00	2.91%	0.000	0.000	0	0	0.00
light oil	46	0.003	0.00952	0.73	0.007	0.03	1.66%	0.000	0.001	0.001134	0.014287	0.36
heavy oil	0	0.0009	0	0.29	0.000	0.00	2.91%	0.000	0.000	0	0	0.00
Relief Valve:			0	0.29	37.50		2.91%	0.000	0.000	0	0	0.00
gas/vapor	4	0.04	0.011037681	0.29	0.003	0.01	2.91%	0.000	0.001	0.001315	0.016565	0.42
Connectors:	4		0	0.29			2.91%	0.000	0.000	0	0	0.00
gas/vapor	67	0.003	0.013866087	0.29	0.004	0.02	2.91%	0.000	0.002	0.001652	0.02081	0.52
light oil	34	0.007	0.016418551	0.73	0.012	0.05	1.66%	0.000	0.001	0.001956	0.024641	0.62
heavy oil	0	0.0003	0	0.29	0.000	0.03	2.91%	0.000	0.000	0	0	0.00
Other	1	0.3	0.020695652	0.29	0.006	0.03	1.66%	0.000	0.002	0.002466	0.03106	0.78
				Totals	0.069	0.330		0.005	0.023	0.019	0.248	6.231

### Notes:

1. Emission factors and equipment counts taken from 40 CFR 98, subpart W.

2	Light oil is defined as having API gravity greater than or equal to 20 degrees API.
3	Vapors emitted from das service equipment assumed to be same as produced das

3.	Vapors emitted from gas service equipment assumed to be same as produced gas,
	vapor from liquid service equipment assumed to be the same as flash gas.

Counts taken nom 40 C	i it so, subpait vv.										
gravity greater than or	equal to 20 degrees	API.	Equipment	Count	Valves	Flan	nges	Fittings	prv	Other	
equipment assumed to	be same as produc	ed gas,	wellhead		1	5	10		4	0	1
ent assumed to be the	same as flash gas.		heater treater		0	0	0		0	0	0
	lb/hr	tpy	header		0	0	0		0	0	0
n-hexane	0.00186	0.00814	separator		0	0	0		0	0	
benzene	0.00022	0.00095	meters/piping		0	0	0		0	0	0
ethyl benzene	0.00023	0.00102	compressor		0	0	0		0	4	0
toluene	0.00004	0.00016	dehydrator		0	0	0		0	0	0
xylene	0.00004	0.00016		total		5	10		4	4	1

### Truck Loading Emissions Calculations 30-Day Average production

Basis: 30 day average production rates

 $L_L = 12.46 * (SPM)/T$ 

(from EPA AP-42 Section 5.2.2.1)

Where:

L<sub>L</sub> = Loading loss, lbs per 1,000 gal of liquid loaded

S = Saturation factor

P = True vapor pressure of liquid, psia
M = Molecular weight of vapors, lb/lb-mole
T = Temperature of bulk liquid loaded, degrees R

#### CRUDE OIL

EPA "S"	True VP	Mol. Wt. Of	Temp.	Sales Volume	Loadin g Rate		Uncontrolled Estimated Emissions,		
Factor	Liquid	Vapors	Liquid	Volume	y Nate	Total Hydrocarbons			
	(psia)	(lb/lb- mole)	(R)	(10 <sup>3</sup> gal/yr)	(gal/hr)	Lı	(lb/hr)	(tpy)	
1.45	5	48.00	545	1,008	16,000	7.96	127.30	4.01	

### PRODUCED WATER

	EPA	True VP	Mol. Wt.	Temp.	Loaded	Loadin	Uncont	rolled Es	timated	
	"S"	of	Of	of	Volume	g Rate	Emissions,		3,	
Calculation	Factor	Liquid	Vapors	Liquid			Total	Total Hydrocarbons		
		(psia)	(lb/lb- mole)	(R)	(10 <sup>3</sup> gal/yr)	(gal/hr)	L	(lb/hr)	(tpy)	
	1.45	0.05	48.00	545	42	16,000	0.08	1.27	0.00	

HAPs tons/yr
Benzene 0.017624
Toluene 0.01745
e-Benzene 0.000673
Xylenes 0.009191
n-hexane 0.119417
0.164355

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### Truck Loading Emissions Calculations, Maximum lbs/hr

 $L_L = 12.46 * (SPM)/T$ 

(from EPA AP-42 Section 5.2.2.1)

Where:

L<sub>L</sub> = Loading loss, lbs per 1,000 gal of liquid loaded

S = Saturation factor

P = True vapor pressure of liquid, psia
M = Molecular weight of vapors, lb/lb-mole
T = Temperature of bulk liquid loaded, degrees R

#### CRUDE OIL

EPA "S" Factor	True VP of Liquid (psia)	Mol. Wt. Of Vapors (Ib/Ib- mole)	of Liquid	Sales Volume (10 <sup>3</sup> gal/hr)	Loadin g Rate (gal/hr)	E	rolled Est missions Hydrocar (lb/hr)	,
1.45	5	48.00	545	16.0	16,000	7.96	127.30	

### PRODUCED WATER

Calculatio

or	"S"	of	Mol. Wt. Of Vapors	of	Loaded Volume		E	rolled Es missions Hydrocai	,
		(psia)	(lb/lb- mole)	(R)	(10 <sup>3</sup> gal/hr)	(gal/hr)	Lı	(lb/hr)	
	1.45	0.05	48.00	545	16.0	16,000	0.08	1.27	

HAPs	lbs/hr
Benzene	0.564848
Toluene	0.559285
e-Benzene	0.021562
Xylenes	0.294576
n-hexane	3.82734
total	5.267611

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### **FLARE PILOT CALCULATIONS**

Emission	Combustion	Capacity			Crit	eria Emiss	ions, tons/	/r		
Unit ID	Source	MMBTUH	PM	PM10	PM2.5	VOC	SO2	HAP		
AA-001a	Flare (Pilot)	0.05	0.000	0.002	0.002	0.021	0.018	0.001	0.000	0.000

Emission	Combustion	Capacity	GHG	Emissions	, metric to	ns/yr	GHG Emissions, short tons/yr						
Unit ID	Source	ммвтин	CO2	CH4	N2O	CO2e	CO2	CH4	N2O	CO2e			
AA-001a	Flare (Pilot)	0.05	23.223	0.000	0.000	23.246	25.59	0.00	0.00	25.62			

### **Gas combustion**

AP-42 Em	nission Factors, lbs/MMBtu	Emission	Factors, kg/MMBtu
ΓSP	0.001863	CO2	53.02
PM10	0.007451	CH4	0.001
PM2.5	0.007451	N2O	0.0001
хОи	0.098039		
0	0.082353		
/OC	0.005392		
502	0.000588		
-IAPs	0.001851		

•

# ATTACHMENT B: BACKUP DOCUMENTATION

```
****
* Project Setup Information
************************************
Project File : Untitled.Ept
Flowsheet Selection : Oil Tank with Separator
Calculation Method : RVP Distillation
Control Efficiency : 100.0%
Known Separator Stream
Geographical Region : All Regions in US
Entering Air Composition : No
Filed Name
                       : Wildcat
Well Name
                       : BOE 16-10
                        : 2017.08.17
Date
Separator Pressure : 24.00[psig]
Separator Temperature : 114.00[F]
Ambient Pressure : 14.70[psia]
Ambient Temperature : 114.00[F]
                      : 114.00[F]
: 0.8700
C10+ MW
                       : 274.00
-- Low Pressure Oil -----
  No. Component mol %
         H2S
                             0.0700
   1
                             0.0000
   2
         02
   3
         CO2
                             0.1700
   4
         N2
                             0.0000
   5
        C1
                             0.6200
                             0.5200
   6
        C2
   7
         C3
                             1.6800
   8
        i-C4
                             0.9900
   9
         n-C4
                             3.1200
         i-C5
   10
                             2.4500
   11
        n-C5
                             3.4200
   12
        С6
                             4.4300
                             8.8900
   13
        C7
   14
         C8
                           18.5800
   15
        C9
                             8.7200
        C10+
                           36.2600
   16
                           0.5300
1.9700
0.1900
        Benzene
   17
   18
         Toluene
        E-Benzene
Xylenes
   19
   20
                            2.5500
   21
         n-C6
                             4.8400
         224Trimethylp
                             0.0000
-- Sales Oil ------
Production Rate : 100[bbl/day]
Days of Annual Operation : 365 [days/year]
API Gravity : 46.0
Reid Vapor Pressure : 5.00[psia]

    Calculation Results

-- Emission Summary -----
          Uncontrolled Uncontrolled
Item
```

VOCs, C3+ 50.597 11.552 Uncontrolled Recovery Info. Vapor 2.6300 [MSCFD] [MSCFD] HC Vapor 2.4800 GOR 26.30 [SCF/bbl] Uncontrolled Uncontrolled No Component [ton/yr] [lb/hr] H2S 0.682 0.156 0.000 2 02 0.000 2.278 0.000 3.032 3 CO2 0.520 4 N2 0.000 5 C1 0.692 4.699 14.401 4.854 C2 1.073 C3 3.288 i-C4 8 1.108 11.178 4.658 5.041 2.643 2.325 2.011 0.420 0.000 2.552 9 n-C4 10 i-C5 1.063 11 n-C5 1.151 12 C6 13 C7 0.603 0.531 14 C8 0.459 15 C9 0.096 16 C10+ 0.000 0.210 17 Benzene 0.048 0.298 18 Toluene 0.068 19 E-Benzene 0.003 20 Xylenes 0.147 21 n=C6 2.400 0.034 2.400 21 n-C6 0.548 22 224Trimethylp 0.000 0.000 Total 61.289 13.993 -- Stream Data ------No. Component MW LP Oil Flash Oil Sale Oil Flash Gas W&S Gas Total Emissions mol % mol % 0.0404 0.0045 0.0000 0.0000 mol % mol % 0.0700 H2S 34.80 1.3134 1.9220 1.5818 1 0.0000 0.0000 2 02 32.00 0.0000 0.1700 CO2 44.01 0.0565 0.0002 4.9447 3.0026 4.0881 3 0.0000 0.6200 0.0000 0.1006 4 N2 28.01 0.0000 0.0000 0.0000 0.0000 0.0000 22.4727 5.3633 5 C1 16.04 14.9261 C2 30.07 0.5200 0.2475 0.0077 11.9841 12.7960 12.3422 1.2461 0.8715 C3 44.10 1.6800 0.6349 19.9346 33.2195 25.7943 i-C4 0.7470 5.9772 7.3806 6.5962 58.12 0.9900 8 3.1200 2.8556 2.3899 2.5970 2.3352 16.3878 9 n-C4 58.12 14.2431 15.1891 1C i-C5 72.15 2.4500 4.9773 5.2541 5.0994 11 n-C5 72.15 3.4200 3.3727 3.3291 5.4098 5.6562 5.5185 4.4770 9.0569 12 C6 4.4300 4.5143 2.4532 2.5253 2.4850 86.16 1.9231 100.20 8.8900 13 C7 9.1932 1.8698 1.8933 114.23 18.5800 18.9881 19.3232 1.4110 1.4564 1.4310 14 C8 128.28 8.7200 166.00 36 2600 8.7200 8.9211 36.2600 37.1218 9.0862 0.2595 0.2825 0.2696 15 C9 37.8314 0.0000 16 C10+ 0.0000 0.0000 17 Benzene 78.11 0.5300 0.5376 0.5438 0.2092 0.2153 0.2119 2.0108 0.1943 18 Toluene 92.13 1.9700 2.0443 0.2517 0.2595 0.2551 0.0093 E-Benzene 0.1978 0.0090 0.0092 19 106.17 0.1900 Xylenes 2.6081 0.1092 20 106.17 2.5500 2.6558 0.1075 0.1114 21 86.18 4.8400 4.9034 4.9544 2.1720 2.2349 2.1998 n-C6

0.0000

162.79

12.94

7.35

0.733

1.0000 0.9768

0.0000

164.91

0.9585

5.77

5.02

0.734

----- E&P TANK

0.0000

46.02

1.59

0.0232

2465.94

0.0000 0.0000

48.41

0.0415

2611.90

1.67

51.43

1.78

0.0183

2796.84

0.0000

160.07

114.24

[BTU/SCF]

[Gas/Air]

[psia] 34.17

[psia] 11.37 0.732

22 224Trimethylp

Stream Mole Ratio

Bubble Pt. @ 100F

RVP @ 100F

Gas Gravity

Heating Value

Spec. Gravity @ 100F

Page 2-----

## Emissions Report - Summary Format Tank Indentification and Physical Characteristics

Identification

User Identification:
City:
Morton
State:
MississIppi
Company:
Pruet Production Co.
Type of Tank:
Horizontal Tank

Description: 250-Gallon Anti-Foam Tank

**Tank Dimensions** 

 Shell Length (ft):
 5.00

 Diameter (ft):
 5.00

 Volume (gallons):
 250.00

 Turnovers:
 1.46

 Net Throughput(gallyr):
 365.00

Is Tank Heated (y/n): N
Is Tank Underground (y/n): N

**Paint Characteristics** 

Shell Color/Shade: White/White Shell Condition Good

**Breather Vent Settings** 

Vacuum Settings (psig): -0.03
Pressure Settings (psig) 0.03

Meterological Data used in Emissions Calculations: Jackson, Mississippi (Avg Atmospheric Pressure = 14.59 psia)

# TANKS 4.0.9d Emissions Report - Summary Format Liquid Contents of Storage Tank

### Anti-Foam Tank - Horizontal Tank Morton, Mississippi

			ily Liquid S perature (de		Liquid Bulk Temp	Vapo	r Pressure	(psia)	Vapor Mol.	Liquid Mass	Vapor Mass	Mol.	Basis for Vapor Pressure
Mixture/Component	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight,	Fract.	Fract.	Weight	Calculations
Tokuene	All	66.19	60.06	72.32	64.24	0.3992	0.3307	0.4793	92.1300			92.13	Option 2: A=6.954, B=1344.8, C=219.48

# TANKS 4.0.9d Emissions Report - Summary Format Individual Tank Emission Totals

### **Emissions Report for: Annual**

Anti-Foam Tank - Horizontal Tank Morton, Mississippi

		Losses(lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Toluene	0.32	7.47	7.79

## Emissions Report - Summary Format Tank Indentification and Physical Characteristics

Identification

User Identification: Corrosion Inhibitor Tank

City: Morton
State: Mississippi

Company: Pruet Production Co.
Type of Tank: Horizontal Tank

Description: 55-Gallon Corrosion Inhibitor Drum(s)

**Tank Dimensions** 

 Shell Length (ft):
 5.00

 Diameter (ft):
 3.00

 Volume (gallons):
 55.00

 Turnovers:
 20.00

 Net Throughput(gal/yr):
 1,095.00

Is Tank Heated (y/n):
Is Tank Underground (y/n):

**Paint Characteristics** 

Shell Color/Shade: White/White Shell Condition Good

**Breather Vent Settings** 

Vacuum Settings (psig): -0.03
Pressure Settings (psig) 0.03

Meterological Data used in Emissions Calculations: Jackson, Mississippi (Avg Atmospheric Pressure = 14.59 psia)

### TANKS 4.0.9d

## **Emissions Report - Summary Format Liquid Contents of Storage Tank**

### Corrosion Inhibitor Tank - Horizontal Tank Morton, Mississippi

Daily Liquid Surf. Bu Temperature (deg F) Tem				Liquid Bulk Temp	Bulk emp Vapor Pressure (psia)		(psia)	Mol. Mass M		Vapor Mass	Mol.	Basis for Vapor Pressure	
Mixture/Component	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight.	Fract.	Fract.	Weight	Calculations
Toluene	All	66.19	60.06	72.32	64.24	0.3992	0.3307	0.4793	92.1300			92.13	Option 2: A=6.954, B=1344.8, C=219.48

### **TANKS 4.0.9d**

### Emissions Report - Summary Format Individual Tank Emission Totals

### **Emissions Report for: Annual**

### Corrosion Inhibitor Tank - Horizontal Tank Morton, Mississippi

		Losses(lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Toluene	0.96	2.74	3.70

## **Emissions Report - Summary Format Tank Indentification and Physical Characteristics**

Identification

User Identification: Emulsion Breaker Tank

City: Morton
State: Mississippi
Company: Pruet production Co.
Type of Tank: Horizontal Tank

Description: 250-Gallon Emulsion Breaker Tank

**Tank Dimensions** 

 Shell Length (ft):
 5.00

 Diameter (ft):
 5.00

 Volume (gallons):
 250.00

 Turnovers:
 2.92

 Net Throughput(gal/yr):
 730.00

Is Tank Heated (y/n):
Is Tank Underground (y/n):

**Paint Characteristics** 

Shell Color/Shade: White/White Shell Condition Good

**Breather Vent Settings** 

Vacuum Settings (psig): -0.03 Pressure Settings (psig) 0.03

Meterological Data used in Emissions Calculations: Jackson, Mississippi (Avg Atmospheric Pressure = 14.59 psia)

### TANKS 4.0.9d

## **Emissions Report - Summary Format Liquid Contents of Storage Tank**

Emulsion Breaker Tank - Horizontal Tank Morton, Mississippi

			ily Liquid S perature (de		Liquid Bulk Temp	Vapo	r Pressure	(psia)	Vapor Mol.	Liquid Mass	Vapor Mass	Mol.	Basis for Vapor Pressure
Mixture/Component	Month	Avg.	Min.	Max,	(deg F)	Avg.	Min.	Max.	Weight	Fract	Fract.	Weight	Calcutations
Tokuene	All	66.19	60.06	72.32	64.24	0.3992	0.3307	0.4793	92.1300			92.13	Option 2: A=6.954, B=1344.8, C=219.48

### **TANKS 4.0.9d**

### **Emissions Report - Summary Format Individual Tank Emission Totals**

**Emissions Report for: Annual** 

Emulsion Breaker Tank - Horizontal Tank Morton, Mississippi

		Losses(lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Taluene	0.64	7.47	8.11

## Emissions Report - Summary Format Tank Indentification and Physical Characteristics

Identification

User Identification: City: State:

Morton Mississippi

Methanol Tank

Company: Type of Tank: Description: Pruet Production Co.
Horizontal Tank
330-Gallon Methanol Tank

**Tank Dimensions** 

 Shell Length (ft):
 5.00

 Diameter (ft):
 5.00

 Volume (gallons):
 330.00

 Turnovers:
 2.21

 Net Throughput(gal/yr):
 730.00

Is Tank Heated (y/n):
Is Tank Underground (y/n):

**Paint Characteristics** 

Shell Color/Shade: White/White Shell Condition Good

**Breather Vent Settings** 

Vacuum Settings (psig): -0.03
Pressure Settings (psig) 0.03

Meterological Data used in Emissions Calculations: Jackson, Mississippi (Avg Atmospheric Pressure = 14.59 psia)

# TANKS 4.0.9d Emissions Report - Summary Format Liquid Contents of Storage Tank

Methanol Tank - Horizontal Tank Morton, Mississippi

	Daily Liquid Surf. Temperature (deg F)		Liquid Bulk Temp	(		(psia)	Vspor Mol.			Mol.	Basis for Vapor Pressure		
Mixture/Component	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max,	Weight.	Fract.	Fract.	Weight	Calculations
Methyl alcohol	All	66.19	60.08	72.32	64.24	1.7478	1,4448	2.1035	32.0400			32.04	Option 2: A=7.897, B=1474.08, C=229.13

# TANKS 4.0.9d Emissions Report - Summary Format Individual Tank Emission Totals

**Emissions Report for: Annual** 

Methanol Tank - Horizontal Tank Morton, Mississippi

	Losses(lbs)				
Components	Working Loss	Breathing Loss	Total Emissions		
Methyl alcohol	0.97	17.15	18.13		

### FESCO, Ltd. 1100 Fesco Ave. - Alice, Texas 78332

For: Pruet Production Co. 217 W. Capital Street Jackson, Mississippi

Sample: Board of Education 16-10 No. 1

First Stage Separator Gas Sampled @ 70 psig & 87 °F

Date Sampled: 08/02/17 Job Number: 73038.001

### **CHROMATOGRAPH EXTENDED ANALYSIS - GPA 2286**

COMPONENT	MOL%	GPM
Hydrogen Sulfide*	< 0.001	
Nitrogen	9.232	
Carbon Dioxide	2.268	
Methane	58.662	
Ethane	11.461	3.079
Propane	9.860	2.729
Isobutane	2.658	0.874
n-Butane	3.610	1.143
2-2 Dimethylpropane	0.000	0.000
Isopentane	0.884	0.325
n-Pentane	0.686	0.250
Hexanes	0.435	0.180
Heptanes Plus	<u>0.244</u>	<u>0.102</u>
Totals	100.000	8.682

### **Computed Real Characteristics Of Heptanes Plus:**

Specific Gravity	3.384	(Air=1)
Molecular Weight	97.54	
Gross Heating Value	5128	BTU/CF

### Computed Real Characteristics Of Total Sample:

Specific Gravity	0.908	(Air=1)
Compressibility (Z)	0.9951	
Molecular Weight	26.18	
Gross Heating Value		
Dry Basis	1353	BTU/CF
Saturated Basis	1331	BTU/CF

\*Hydrogen Sulfide tested on location by: Stain Tube Method (GPA 2377) <0.013 Gr/100 CF, <0.2 PPMV or <0.001 Mol %

Base Conditions: 14.730 PSI & 60 Deg F

Sampled By: (16) Certified: FESCO, Ltd. - Alice, Texas

Analyst: MR Processor: CRP Cylinder ID: G-4061P

David Dannhaus 361-661-7015

FESCO, Ltd. Job Number: 73038.001

### CHROMATOGRAPH EXTENDED ANALYSIS - GPA 2286 TOTAL REPORT

COMPONENT	MOL %	GPM	WT %
Hydrogen Sulfide*	< 0.001		< 0.001
Nitrogen	9.232		9.879
Carbon Dioxide	2.268		3.813
Methane	58.662		35.950
Ethane	11.461	3.079	13.165
Propane	9.860	2.729	16.609
Isobutane	2.658	0.874	5.901
n-Butane	3.610	1.143	8.015
2,2 Dimethylpropane	0.000	0.000	0.000
Isopentane	0.884	0.325	2.436
n-Pentane	0.686	0.250	1.891
2,2 Dimethylbutane	0.017	0.007	0.056
Cyclopentane	0.000	0.000	0.000
2,3 Dimethylbutane	0.042	0.017	0.138
2 Methylpentane	0.140	0.058	0.461
3 Methylpentane	0.076	0.031	0.250
n-Hexane	0.160	0.066	0.527
Methylcyclopentane	0.025	0.009	0.080
Benzene	0.017	0.005	0.051
Cyclohexane	0.021	0.007	0.067
2-Methylhexane	0.023	0.011	0.088
3-Methylhexane	0.020	0.009	0.077
2,2,4 Trimethylpentane	0.000	0.000	0.000
Other C7's	0.029	0.013	0.110
n-Heptane	0.034	0.016	0.130
Methylcyclohexane	0.019	0.008	0.071
Toluene	0.011	0.004	0.039
Other C8's	0.022	0.010	0.093
n-Octane	0.008	0.004	0.035
Ethylbenzene	0.001	0.000	0.004
M & P Xylenes	0.004	0.002	0.016
O-Xylene	0.001	0.000	0.004
Other C9's	0.006	0.003	0.029
n-Nonane	0.002	0.001	0.010
Other C10's	0.001	0.001	0.005
n-Decane	0.000	0.000	0.000
Undecanes (11)	0.000	<u>0.000</u>	0.000
Totals	100.000	8.682	100.000

### Computed Real Characteristics Of Total Sample:

Specific Gravity	0.908	(Air=1)	
Compressibility (Z)	0.9951		
Molecular Weight	26.18		
Gross Heating Value			
Dry Basis	1353	BTU/CF	
Saturated Basis	1331	BTU/CF	